

PEPSE[®]'s Use in Cost/Benefit Decision - Case Studies

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PEPSE'S USE IN COST/BENEFIT DECISIONS

CASE STUDIES

by

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PEPSE software was used to provide the thermal benefit for maintenance decisions. Three cases were described for Beebee Unit 12, a General Electric 80 megawatt net machine with a tandem compound, double-flow reheat turbine and a hydrogen-cooled generator. The steam is supplied by a Combustion Engineering tangentially fired, controlled circulation, reheat steam generator. The cases discussed are; make up losses due to isolation leaks, feedwater relief valve leaks to condenser and low pressure feedwater heater repairs.

The Performance Monitoring Services group uses PEPSE Rev57 on the OS2 platform. The model of Unit 12 was created in Rev54 using General Electric turbines and shapers to match a series of A/E heat balances. That base model was modified to reflect any changes made to the turbine cycle since the original design. The model was then converted to Type 8 turbines. This is referred to as the benchmark model. For the studies described, the condenser (190) was replaced by a HEI condenser and the #3 low pressure heater (280) was changed from a performance mode to a simplified design mode heater. The PEPSE benchmark schematic is included in Appendix A as Figure 1.

Makeup Losses

Station operating staff noticed much larger than normal daily makeup water requirement. Three sources of system leaks were found during unit walk downs. These included; boiler circulating water pump seal leaks, girth header drain valve leaks and superheater header vent valve leaks. The station had makeup flow requirements calculated when the unit was isolated. The benchmark flow was calculated to be 1000 pounds/hour. The system leaks were calculated to be 3750 pounds/hour. Maintenance required a cost/benefit analysis to be done to decide when maintenance should be performed.

To model makeup loss, the benchmark model was modified to include a splitter (362), after the #6 feedwater heater (350), connected to a sink. The PEPSE schematic associated with this case is included in Appendix B as Figure 2. This location is essentially at the same state as the water entering the economizer. Unit makeup goes directly into the condenser. A mixer (7) was added to the #1 heater drain line (10) entering the condenser.

The model was run with stacked cases for 0, 1000 and 3750

pounds per hour makeup water requirements. The BTU/Kwh calculated by PEPSE for the 1000 lb/hr case was subtracted from the heat rate calculated for the 3750 lb/hr case (additional makeup required was 12,000 Gal/day). Conversion to dollars per day using the corporate value of cents per million BTU projected a loss of \$1000 dollars per day at full load.

This method is not meant to yield an exact value. The shortcuts applied included using the feedwater state entering the economizer and using the full load loss applied as a constant for all loads. To obtain a "real" value, the point of system loss would have to be the liquid saturation enthalpy at the drum pressure. Methods to model the enthalpy difference are available but were not chosen because the split between the girth header leaks and the header vent leaks was not known. This assumption tends toward a conservative answer. The second shortcut of using the PEPSE full load BTU/Kwh loss for the whole load range also adds an error to the analysis. The unit capacity factor during the study period was 10% lower than the PEPSE benchmark model. This assumption tends to give a higher cost to the makeup loss. The two shortcuts applied together would cancel.

The \$1000 per day value was used by the Maintenance, Operations and Power Control Groups to evaluate whether it was cost effective to remove the unit from service, and drain the boiler to repair these valves. The work was deferred to a period of economic reserve for repair. The Special Output Table of Specified Variables for the Benchmark and 12000 Gal/Day Makeup cases are in Appendix B along with the .JOB file.

Feedwater Relief Valve Leaks to Condenser

The water side pressure relief valves on numbers 4 and 6 feedwater heaters were noted by plant operators to be leaking. PMS was asked to determine the savings if those leaks were repaired. The model used was the same as in the Makeup study previously discussed. Splitters were added in the feedwater lines entering both #4 and #6 heaters. The flows were diverted to a mixer in the #1 heater drain line to the condenser (points E and F entering 510 in the schematic).

The amount of flow leaking by was not known. The inside diameter of the outlet line was determined from the piping specification. The valve specification noted a smaller internal opening than the line to the reclaim tank (modelled as the mixer 510). The maximum flow through the line was determined using Cameron's Hydraulic Data for the smaller opening and compared to the valve specification flow. Both heater relief valves are identical and the pressure drop between #4 and #6 heater is negligible compared to feedwater pressure; the maximum flow was determined to be 1600 pounds/hour. More complex modelling is possible with PEPSE valves and stream options; however, for this evaluation, that degree of detail was unnecessary. The difference in turbine heat rate between the Benchmark and the leaking case was calculated to be 7 BTU/kWh. The repair was deferred. Shortly after the determination not to derate the unit and repair the relief valves, a leak developed in one of the valves, necessitating a

derating. A comparison of turbine heat rate pre and post repair made to determine the effect of the repair compared to the model. The savings were calculated to be 5 BTU/kw.

Low Pressure Feedwater Heater Repairs

Unit 12's low pressure heaters share a common shell located in the neck of the condenser. The #3 heater has over 15% of its tubes plugged because of leaks. The steam side partition between the #3 and #2 heaters has been known to leak. The test data reduction model routinely used by PMS does not take this leakage into consideration. The Maintenance Group will be doing a major turbine overhaul late in 1993 and needed to evaluate the benefit of retubing the heater. Through eddy current testing, it was determined that an additional 6 tubes should be plugged. PMS was asked to determine the thermal cost associated; with the present number of plugged tubes, and with additional #3 heater surface area reduction to decide the course of action. The need to repair the shell partition was also mentioned as necessary to avoid premature tube failure if the heater were retubed. That benefit also had to be determined.

The PEPSE benchmark model was modified by including the #3 heater simplified design submodel and by changing the condenser from Performance mode to HEI mode. The heater submodel was created from the vendor specification sheet. The #3 heater is a dry, forward draining heater with a desuperheating section. The stacked cases to determine the effect of tubes plugged used actual TTD values with 22 tubes plugged, with an additional 2 degree deviation in TTD (additional 6 tubes plugged) as compared to design. The heater costs 7 BTU/kWh at full load with the 22 plugged tubes. The additional 6 plugs will add 3 BTU/kWh more. The 10 BTU/kWh loss does not include heater shell bypassing or additional auxiliary use required as a result of the increased feedwater pressure differential. The increased auxiliary requirement was felt to be minimal and not calculated.

Identifying the cost of the heater shell partition leak could further reduce the time required to break even. The common bundle for the low pressure heaters does not allow testing to evaluate steam side leaks. The problem becomes more unknowns than equations. To provide PEPSE with data, an energy balance around the #3 and #2 heaters was made. The leak between the heaters was assumed to be small with respect to the extraction flow, which made the calculation of an extraction flow ratio. The design extraction flow ratio was calculated using the full load A/E heat balances and compared to the performance data acquisition scan which calculates a real time turbine heat rate based on feedwater flow. The difference was 9% or 1900 pounds/hour. Another test done during outages is a static pressure test. The #3 heater is flooded, the level is recorded over time and the amount of water used to flood the heater is known. That rate was rounded down to 1000 pounds/hour. The static pressure test was used as a sanity check on the ratio calculation. The higher number was used based on; the higher pressure differential between the heaters during operation compared to the static test, and the density difference between

steam and water.

The model was run with 1900 pounds/hour shell bypassing between #3 and #2 heater. The additional loss was calculated to be 2 BTU/Kwh. The simple payback to retube the heater is less than 3 years. The payback on repairing the shell partition is dependent on the repair cost. The Special Output Table of Specified Variables for the Benchmark, #3 Heater As Is, #3 heater with additional tubes plugged and the shell partition bypassing cases are in Appendix C.

Summary

PEPSE software was used to provide the thermal benefit for maintenance decisions. The cases discussed are; make up losses due to isolation leaks, feedwater relief valve leaks to condenser and low pressure feedwater heater repairs. The methodology used in the analysis and the results were reported.

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APPENDIX A

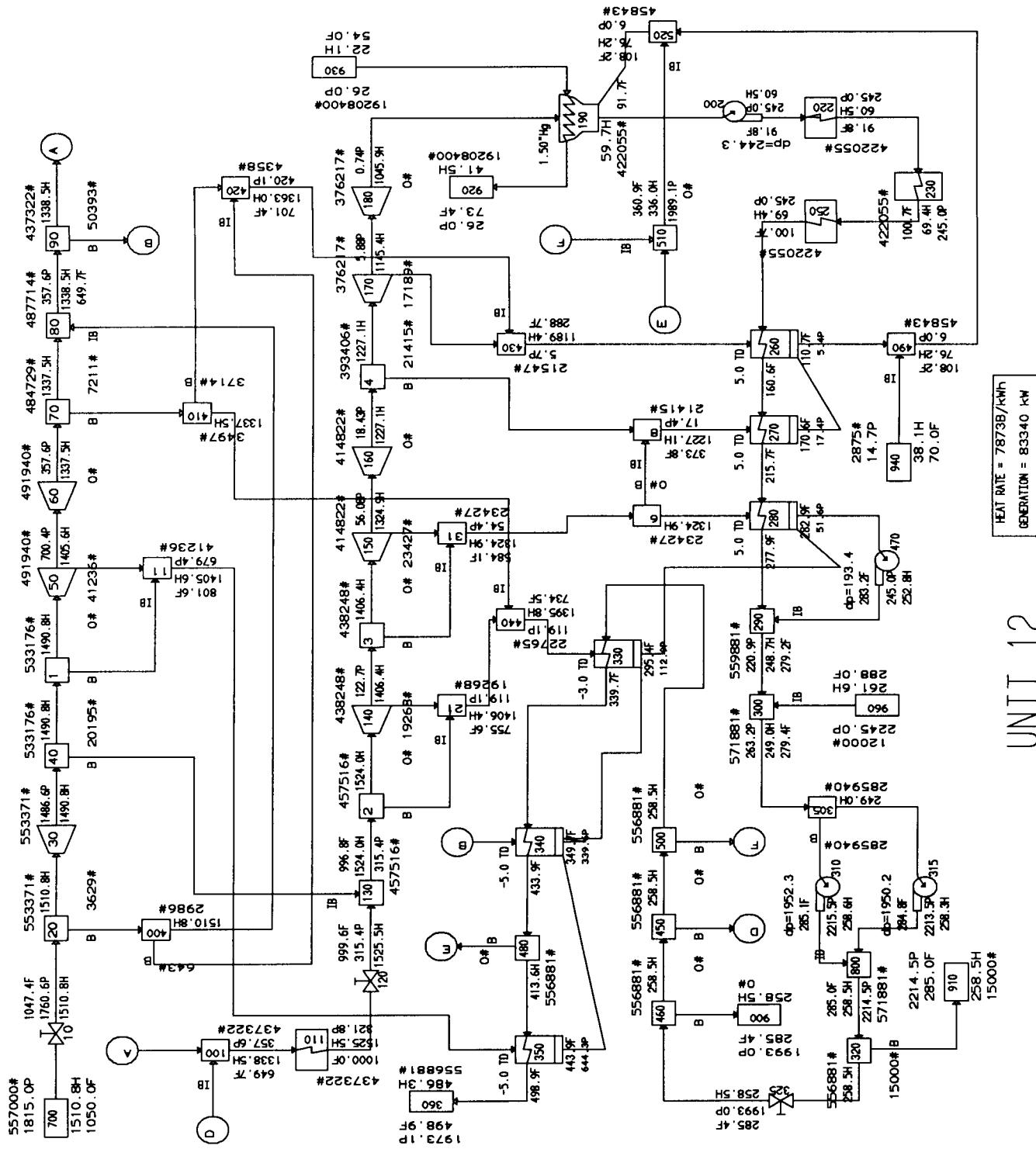


Figure 1. PEPSE Benchmark

APPENDIX B

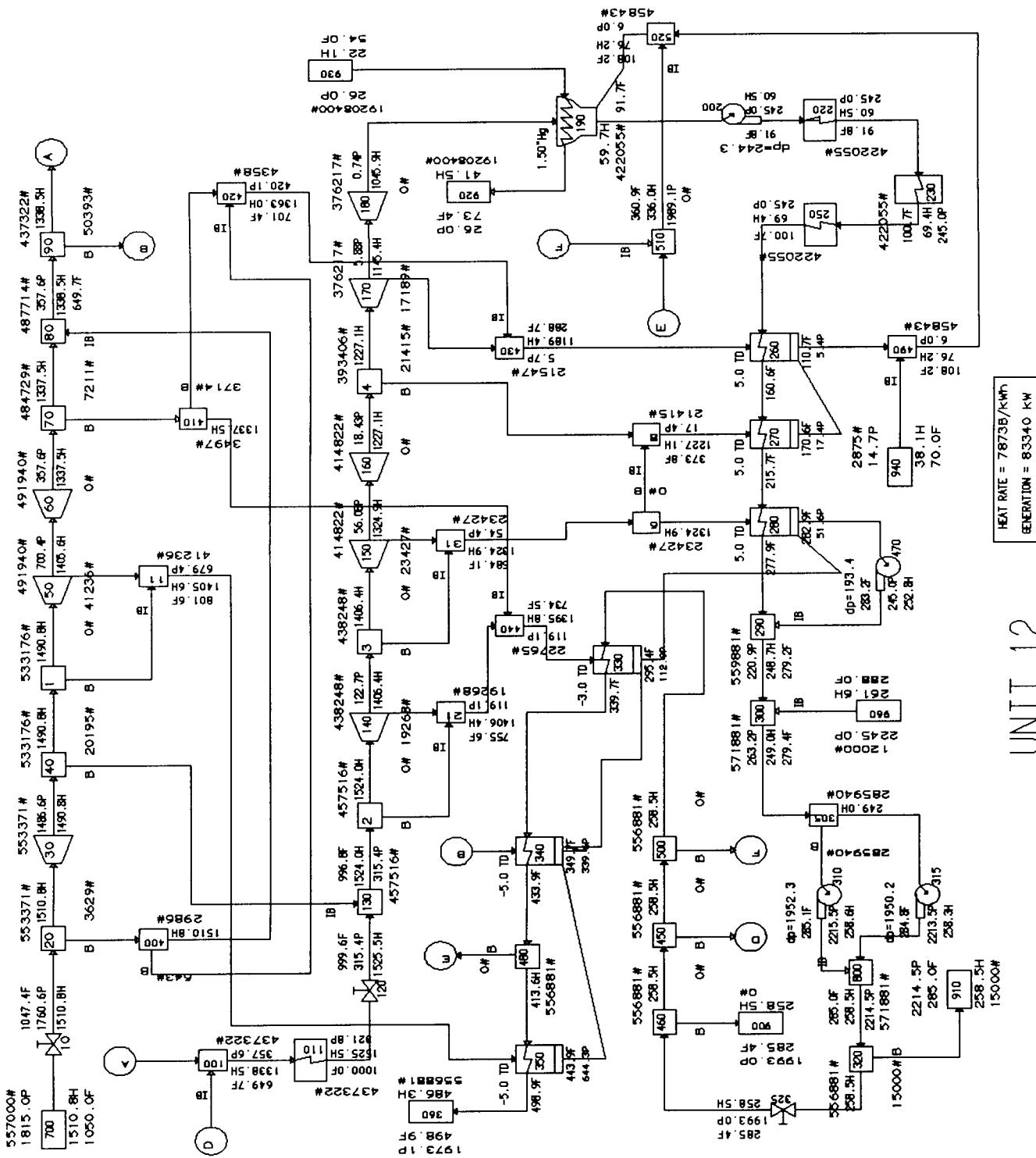


Figure 2. Makeup Loss Case Schematic

SPECIAL OUTPUT TABLE OF SPECIFIED VARIABLES

INDEX	DESCRIPTION	VARIABLE (ID)	VALUE
1	GROSS TURBINE CYCLE POWER OUTPUT (MW)	BKGROS(0)	83.3974
2	GROSS TURBINE CYCLE HEAT RATE (BTU/KWH)	GPVB (16)	7823.3636
3	GROSS TURBINE CYCLE THERMAL EFFIC. (%)	GPVB (35)	43.6147
4	H.P. TURBINE SECTION EFFIC. (%)	GPVB (36)	83.6030
5	I.P. TURBINE SECTION EFFIC. (%)	GPVB (37)	89.0878
6	L.P. TURBINE SECTION EFFIC. (%)	GPVB (38)	76.0634
7	MAIN STEAM FLOW (#/HR)	WW (5)	557000.0000
8	MAIN STEAM PRESSURE (PSIA)	PP (5)	1815.0060
9	MAIN STEAM TEMPERATURE (DEG-F)	TT (5)	1050.0000
10	1ST STAGE PRESSURE (PSIA)	PP (35)	1486.6454
11	10TH STAGE PRESSURE (PSIA)	PP (65)	357.4371
12	COLD REHEAT PRESSURE (PSIA)	PP (95)	357.4371
13	COLD REHEAT TEMPERATURE (DEG-F)	TT (95)	649.6611
14	HOT REHEAT PRESSURE (PSIA)	PP (115)	321.7292
15	HOT REHEAT TEMPERATURE (DEG-F)	TT (115)	1000.0060
16	I.P. INLET PRESSURE (PSIA)	PP (136)	315.2946
17	I.P. EXHAUST PRESSURE (PSIA)	PP (165)	18.4280
18	CONDENSER BACK PRESSURE (IN-HG)	PP (195)	0.4936
19	CIRC. WATER INLET TEMPERATURE (DEG-F)	TT (932)	54.0060
24	#4 FEEDWATER HEATER PRESSURE DROP	PDFW (330)	0.0000

SPECIAL OUTPUT TABLE OF SPECIFIED VARIABLES

INDEX	DESCRIPTION	VARIABLE (ID)	VALUE
1	GROSS TURBINE CYCLE POWER OUTPUT (MW)	BKGROS(0)	83.2459
2	GROSS TURBINE CYCLE HEAT RATE (BTU/KWH)	GPVB (16)	7836.6362
3	GROSS TURBINE CYCLE THERMAL EFFIC. (%)	GPVB (35)	43.5409
4	H.P. TURBINE SECTION EFFIC. (%)	GPVB (36)	83.6056
5	I.P. TURBINE SECTION EFFIC. (%)	GPVB (37)	89.0889
6	L.P. TURBINE SECTION EFFIC. (%)	GPVB (38)	76.0776
7	MAIN STEAM FLOW (#/HR)	WW (5)	557000.0000
8	MAIN STEAM PRESSURE (PSIA)	PP (5)	1815.0000
9	MAIN STEAM TEMPERATURE (DEG-F)	TT (5)	1050.0000
10	1ST STAGE PRESSURE (PSIA)	PP (35)	1486.6439
11	10TH STAGE PRESSURE (PSIA)	PP (65)	356.8394
12	COLD REHEAT PRESSURE (PSIA)	PP (95)	356.8394
13	COLD REHEAT TEMPERATURE (DEG-F)	TT (95)	649.3070
14	HOT REHEAT PRESSURE (PSIA)	PP (115)	321.1911
15	HOT REHEAT TEMPERATURE (DEG-F)	TT (115)	1000.0000
16	I.P. INLET PRESSURE (PSIA)	PP (136)	314.7673
17	I.P. EXHAUST PRESSURE (PSIA)	PP (165)	18.4280
18	CONDENSER BACK PRESSURE (IN-HG)	PP (195)	0.4931
19	CIRC. WATER INLET TEMPERATURE (DEG-F)	TT (932)	54.0000
24	#4 FEEDWATER HEATER PRESSURE DROP	PDFW (330)	0.0000

LISTING OF INPUT DATA FOR CASE 1

```

1   010001  132 * 132 column output
2   *
3   *      PEPSE USER : ADMIN
4   *      DATE : 03/29/93
5   *      TIME : 07:37
6   *      MODEL FILE ID : BB12
7   *      JOB FILE ID : \EASEPLUS\DEMO\bb12.JOB
8   *      RESULTS FILE ID : \EASEPLUS\DEMO\bb12.OUT
9   *
10 =      BEEBEE STATION - UNIT # 12 - BENCHMARK FOR TEST 06/15/90 - 83.323
11 *
12 *
13 *
14 ****
15 *      GENERIC INPUT DATA
16 ****
17 *
18 *      CYCLE FLAGS
19 010200  2   3   1   1   1   0   0.   0.
20 010201  3
21 *
22 *      GENERATOR #1 FLAGS AND DATA
23 011010  1   2   1   0   3600  96000.  0.85  44.7  44.7   0.
24 011011  360. 1190.   0.
25 *
26 *      CYCLE CONVERGENCE DATA
27 012000  50   50.   50.   0.   0.   0.   0   100000.
28 *
29 *      PEPSE OUTPUT SUPPRESSION CARDS
30 *
31 020000  NOPRNT PRINT
32 020003  PRINT
33 020006  PRINT
34 020007  PRINT
35 020008  PRINT
36 020009  PRINT
37 020010  PRINT
38 020020  PRINT
39 020023  PRINT
40 020038  PRINT
41 020039  PRINT
42 020076  PRINT
43 *
44 *      SPECIAL INPUT/OUTPUT OUTPUT TABLE FORMAT
45 890000  1   1
46 *
47 *
48 ****
49 *      GEOMETRY CARDS
50 ****
51 *
52 500460  1     U   50   I
53 500470  1     B   11   IB
54 501360  2     U   140  I
55 501370  2     B   21   IB
56 501460  3     U   150  I
57 501470  3     B   31   IB
58 501670  4     U   170  I
59 501570  4     B   8    IA
60 501560  5     U   280  S
61 500610  5     B   8    IB
62 500100  7     U   520  IA
63 501580  9     U   270  S
64 500090  9     U   7    IB
65 500150  10    U   20   I
66 500540  11    U   350  S
67 500250  20    U   30   I
68 500220  20    B   400  I
69 501440  21    U   440  IA
70 500350  30    U   40   I
71 501540  31    U   6    I
72 500450  40    U   1    I
73 500420  40    B   130  IB
74 500550  50    U   60   I
75 500510  50    E   11   IA
76 500650  60    U   70   I
77 500750  70    U   80   IA
78 500710  70    B   410  I
79 500850  80    U   90   I
80 500950  90    U   100  IA
81 500910  99    B   340  S
82 501050  100   U   110  T

```

83	501150	110	I	120	I
84	501250	120	U	130	IA
85	501350	130	U	2	I
86	501450	140	U	3	I
87	501410	140	E	21	IA
88	501550	150	E	160	I
89	501510	150	E	31	IA
90	501650	160	U	4	I
91	501750	170	U	180	I
92	501710	170	E	430	IA
93	501850	180	U	190	S
94	501920	190	T	920	I
95	501950	190	D	200	I
96	502050	200	U	220	T
97	502250	220	T	230	T
98	502350	230	T	250	T
99	502550	250	T	260	T
100	502650	260	T	270	T
101	502690	260	D	490	IA
102	502750	270	T	280	T
103	502790	270	D	260	D
104	502850	280	T	290	IA
105	502890	280	D	470	I
106	502950	290	U	300	IA
107	503050	300	U	305	I
108	503120	305	U	315	I
109	503070	305	B	310	I
110	503130	310	U	800	IB
111	503170	315	U	800	IA
112	503250	320	U	325	I
113	503220	320	B	910	I
114	503260	325	U	460	I
115	503350	330	T	340	T
116	503390	330	D	280	D
117	503450	340	T	480	I
118	503490	340	D	330	D
119	503550	350	T	362	I
120	503590	350	D	340	D
121	503560	362	U	360	I
122	503630	362	B	361	I
123	504020	400	U	80	IB
124	504030	400	B	420	IB
125	504110	410	U	440	IB
126	504120	410	B	420	IA
127	504220	420	U	430	IB
128	504310	430	U	260	S
129	504410	440	U	330	S
130	503280	450	U	500	I
131	504630	450	B	100	IB
132	500070	460	U	450	I
133	504620	460	B	900	I
134	504720	470	U	290	IB
135	503460	480	U	350	T
136	504850	480	B	510	IA
137	504900	490	U	7	IA
138	503290	500	U	330	T
139	505050	500	B	510	IB
140	505150	510	U	520	IB
141	505250	520	U	190	D
142	500050	700	U	10	I
143	503190	800	U	320	I
144	509320	930	U	190	T
145	509420	940	U	490	IB
146	509620	960	U	300	IB

147

*

148

*

149 ***** SPECIAL STREAM SPECIFICATIONS *****

150 * ***** SPECIAL STREAM SPECIFICATIONS *****

151 *

152 *

153 ***** STREAM TYPES 1 - 7 *****

154 *

155 *

156 600540 2 0.0516 0. 0. 0. 0. 0.

157 *

158 600910 2 0.0503 0. 0. 0. 0. 0.

159 *

160 601540 2 0.0524 0. 0. 0. 0. 0.

161 * #2 HEATER EXTRACTION

162 601570 2 0.082 0. 0. 0. 0. 0.

163 *

164 604310 2 0.0521 0. 0. 0. 0. 0.

165 *

166 604410 2 0.0522 0. 0. 0. 0. 0.

167 *

168 ***** STREAM FLOW OPTION *****

169 *

170 *

```

172 *****
173 * COMPONENT DATA
174 *****
175 *
176 ***** TURBINES
177 *
178 *
179 700300 8 1 0 0 1 0
180 + 1 3 0. 0. 0. 0.
181 + 0. 0 0. 0. 0. 0.
182 700303 0.77898 10207.9
183 700309 1760.55 1510.79 553371. 0. 0. 0. 0. 0. 0.
184 *
185 700500 8 1 1 1 2 0
186 + 1 3 0.03 0. 0. 0.
187 + 0. 0 0. 0. 0. 0.
188 700503 0.81974 18708.3
189 *
190 700600 8 1 3 0 2 0
191 + 1 1 0. 0. 0.
192 + 0. 0 0. 0. 0. 0.
193 700601 0.83112 357.346
194 *
195 701400 8 1 0 1 4 0
196 + 1 3 0.03 0. 0.
197 + 0. 0 0. 0. 0. 0.
198 701403 0.87128 95532.6
199 701409 315.214 1524.01 457225. 0. 0. 0. 0. 0. 0.
200 *
201 701500 8 1 1 1 4 0
202 + 1 3 0.03 0. 0.
203 + 0. 0 0. 0. 0. 0.
204 701503 0.85763 183621.
205 *
206 701600 8 1 3 0 5 0
207 + 1 1 0. 0. 0.
208 + 0. 0 0. 0. 0. 0.
209 701601 0.87403 18.428
210 *
211 701700 8 1 1 1 4 0
212 + 2 3 0.03 0. 0.
213 + 0. 0 0. 0. 0. 0.
214 701703 0.89719 1.257E+6
215 701709 18.428 1227.16 392716. 0. 0. 0. 0. 0. 0.
216 *
217 701800 8 1 3 0 4 0
218 + 2 1 0. 0. 26.175
219 + 0. 0 0. 0. 0. - 0.
220 701801 0.89413 0.737
221 *
222 ***** CONDENSERS AND FEEDWATER HEATERS
223 *
224 * Main Condenser
225 701900 10 1 5 0. -1.5
226 701905 1 0.777 0.875 336. 7020. 2 0. 0.
227 * #1 Feedwater Heater
228 702600 16 1 170 2 0. 5. 10.
229 702601 0. 0. 0. 0. 0. 0.
230 702602 0. 0. 0. 0. 0. 0.
231 * #2 Feedwater Heater
232 702700 16 0 4 2 0. 5. 10.
233 702701 0. 0. 0. 0. 0. 0.
234 702702 0. 0. 0. 0. 0. 0.
235 * #3 Feedwater Heater
236 702800 17 1 150 2 0. 5.
237 702801 0. 0. 0. 0. 0. 0.
238 702802 0. 0. 0. 0. 0. 0.
239 * #4 Feedwater Heater
240 703300 18 1 140 2 0. -3. 10.
241 703301 0. 0. 0. 0. 0. 0.
242 703302 0. 0. 0. 0. 0. 0.
243 * #5 Feedwater Heater
244 703400 18 1 90 2 0. -5. 10.
245 703401 0. 0. 0. 0. 0. 0.
246 703402 0. 0. 0. 0. 0. 0.
247 * #6 Feedwater Heater
248 703500 18 0 50 2 0. -5. 10.
249 703501 0. 0. 0. 0. 0. 0.
250 703502 0. 0. 0. 0. 0. 0.
251 *
252 ***** HEAT EXCHANGERS
253 *
254 * Reheater
255 701100 25 2 1000.
256 701101 0.0999 0. 0. 0. 0.
257 *
258 702200 27 0. 0. 0. 0.

```

259 *
 260 702300 27 3.7543E+6 0. 0. 0.
 261 *
 262 702500 27 0. 0. 0. 0.
 263 *
 264 ***** SOURCES, SINKS, AND VALVES
 265 *
 266 * MAKE UP FLOW
 267 700090 31 85. 15. 1000. 0. 0. 0
 268 *
 269 707000 33 1050. 1815. 557000. 0. 0. 0
 270 *
 271 709300 31 54. 26. 1.92084E+7 0. 0. 0
 272 *
 273 709400 31 70. 14.7 2875. 0. 0. 0
 274 *
 275 709600 31 288. 2245. 12000. 0. 0. 0
 276 *
 277 703600 32
 278 * blowdown
 279 703610 30
 280 *
 281 709000 30
 282 *
 283 709100 30
 284 *
 285 709200 30
 286 *
 287 700100 35 -2. -2. -2. 0.3 1815. 1510.9 557000.
 288 *
 289 701200 34 0.02 0. 0.
 290 *
 291 703250 34 0.1 0. 0.
 292 *
 293 ***** PUMPS, COMPRESSORS, AND FANS
 294 *
 295 *
 296 702000 41 245. 0. 0. 0.
 297 702001 0. 0. 0. 0. 0. 0.
 298 *
 299 703100 41 2208. 0.87 1. 0.7
 300 703101 0. 0. 0. 0. 0. 0.
 301 *
 302 703150 41 2208. 0.87 1. 0.7
 303 703151 0. 0. 0. 0. 0. 0.
 304 *
 305 704700 41 245. 0. 0. 0.
 306 704701 0. 0. 0. 0. 0. 0.
 307 *
 308 ***** MIXERS
 309 *
 310 * PARTITION LEAKAGE BETWEEN #'S 3 AND 2 HE
 311 700080 50 1 0.
 312 *
 313 700110 50 1 0.
 314 *
 315 700210 50 1 0.
 316 *
 317 700310 50 1 0.
 318 *
 319 701000 50 1 0.
 320 *
 321 701300 50 1 0.
 322 *
 323 704200 50 0 0.
 324 *
 325 704900 50 0 0.
 326 * RECLAIM TANK
 327 705100 50 0 0.
 328 * RECLAIM TANK
 329 705200 50 0 0.
 330 *
 331 708000 50 0 0.
 332 *
 333 700070 50 0 0.
 334 *
 335 700600 50 1 0.
 336 *
 337 702900 50 0 0.
 338 *
 339 703000 50 0 0.
 340 *
 341 704300 50 1 0.
 342 *
 343 704400 50 1 0.
 344 *
 345 ***** SPLITTERS

347 *
 348 703050 63 0. 0.5
 349 * blowdown
 350 703620 61 0. 1000.
 351 *
 352 704000 68 643. 52.1272 0.
 353 * #6 HEATER RELIEF VALVE
 354 704800 61 0. 0.
 355 *
 356 700010 61 0. 0.
 357 *
 358 700020 61 0. 0.
 359 *
 360 700030 61 0. 0.
 361 * #2 EXTRACTION
 362 700040 60 0. 21827. 0. 0 0.
 363 700041 1
 364 * PARTITION PLATE BY-PASSING FROM #3 TO #2
 365 700060 60 0. 0. 0. 0 0.
 366 *
 367 700200 68 3629. 57.7267 0.
 368 *
 369 700400 64 386.635 0. 0.
 370 *
 371 700700 64 505.519 0. 0.
 372 *
 373 700900 60 0. 50554. 0. 0 0.
 374 *
 375 703200 61 0. 15000.
 376 *
 377 704100 64 783.775 0. 0.
 378 * REHEAT SPRAY
 379 704500 61 0. 0.
 380 *
 381 704600 61 0. 0.
 382 * #4 HEATER RELIEF VALVE
 383 705000 61 0. 0.
 384 *
 385 *
 386 *****
 387 * SPECIAL FEATURES
 388 *****
 389 *
 390 ***** SCHEDULES
 391 *
 392 *
 393 800100 'H2 COOLER HEAT INPUT VS. THROTTLE FLOW '
 394 * X VALUES
 395 810100 139000. 201000. 265000.- 328500. 389000.
 396 810101 442000. 500500. 557000.
 397 * Z AND Y VALUES
 398 810110 0. 388.000000 445.000000 518.000000 596.000000 687.000000
 399 810111 788.000000 959.000000 1100.000000
 400 * Y, X, AND Z MULTIPLIERS
 401 820100 3412.13 0. 0.
 402 *
 403 800200 'TOT GEN ELEC LOSS VS. GEN GROSS OUTPUT '
 404 * X VALUES
 405 810200 21.53 31.823 42.146 51.979 60.983
 406 810201 68.427 76.202 83.27
 407 * Z AND Y VALUES
 408 810210 0. 478.000000 535.000000 608.000000 686.000000 777.000000
 409 810211 878.000000 1049.000000 1190.000000
 410 *
 411 800300 'GOV. STAGE EFF. VS. EQ. THR. FLOW RATIO '
 412 * X VALUES
 413 810300 0.36083 0.47572 0.58972 0.69833 0.79347
 414 810301 0.89849 1.
 415 * Z AND Y VALUES
 416 810310 0. 0.401950 0.454930 0.516480 0.583790 0.647530
 417 810311 0.720250 0.778980
 418 *
 419 800400 '6TH STAGE EFF. VS. EQ. THR. FLOW RATIO '
 420 * X VALUES
 421 810400 0.36083 0.47572 0.58972 0.69833 0.79347
 422 810401 0.89849 1.
 423 * Z AND Y VALUES
 424 810410 0. 0.869180 0.865910 0.851990 0.837010 0.824660
 425 810411 0.817910 0.819740
 426 *
 427 800500 '10TH STAGE EFF. VS. EQ. THR. FLOW RATIO '
 428 * X VALUES
 429 810500 0.36083 0.47572 0.58972 0.69833 0.79347
 430 810501 0.89849 1.
 431 * Z AND Y VALUES
 432 810510 0. 0.800480 0.814440 0.822420 0.829060 0.832580
 433 810511 0.833670 0.831110
 434 *

435 800600 '15TH STAGE EFF. VS. EQ. THR. FLOW RATIO'
 436 * X VALUES
 437 810600 0.36083 0.47572 0.58972 0.69833 0.79347
 438 810601 0.89849 1.
 439 * Z AND Y VALUES
 440 810610 0. 0.887270 0.881460 0.878960 0.875980 0.873630
 441 810611 0.871510 0.871290
 442 *
 443 800700 '18TH STAGE EFF. VS. EQ. THR. FLOW RATIO'
 444 * X VALUES
 445 810700 0.36083 0.47572 0.58972 0.69833 0.79347
 446 810701 0.89849 1.
 447 * Z AND Y VALUES
 448 810710 0. 0.869290 0.867190 0.864450 0.865410 0.865060
 449 810711 0.862140 0.857630
 450 *
 451 800800 '21ST STAGE EFF. VS. EQ. THR. FLOW RATIO'
 452 * X VALUES
 453 810800 0.36083 0.47572 0.58972 0.69833 0.79347
 454 810801 0.89849 1.
 455 * Z AND Y VALUES
 456 810810 0. 0.876040 0.870730 0.870330 0.867480 0.867270
 457 810811 0.869380 0.874030
 458 *
 459 800900 '23RD STAGE EFF. VS. EQ. THR. FLOW RATIO'
 460 * X VALUES
 461 810900 0.36083 0.47572 0.58972 0.69833 0.79347
 462 810901 0.89849 1.
 463 * Z AND Y VALUES
 464 810910 0. 0.897780 0.896280 0.896340 0.895970 0.895980
 465 810911 0.896160 0.897190
 466 *
 467 801000 '25TH STAGE EFF. VS. EQ. THR. FLOW RATIO'
 468 * X VALUES
 469 811000 0.36083 0.47572 0.58972 0.69833 0.79347
 470 811001 0.89849 1.
 471 * Z AND Y VALUES
 472 811010 0. 0.896960 0.895000 0.894550 0.893900 0.893650
 473 811011 0.893570 0.894140
 474 *
 475 801100 '6 EXTR. PRESS. DROP CONST. VS. THR. FLOW'
 476 * X VALUES
 477 811100 201000. 265000. 328500. 389000. 442000.
 478 811101 500500. 557000.
 479 * Z AND Y VALUES
 480 811110 0. 0.055800 0.055100 0.053900 0.052800 0.052000
 481 811111 0.051400 0.051600
 482 *
 483 801200 '5 EXTR. PRESS. DRGP CONST. VS. TRH. FLOW'
 484 * X VALUES
 485 811200 201000. 265000. 328500. 389000. 442000.
 486 811201 500500. 557000.
 487 * Z AND Y VALUES
 488 811210 0. 0.050200 0.050300 0.050200 0.049600 0.049700
 489 811211 0.050000 0.050300
 490 *
 491 801300 '3 EXTR. PRESS. DROP CONST. VS. THR. FLOW'
 492 * X VALUES
 493 811300 201000. 265000. 328500. 389000. 442000.
 494 811301 500500. 557000.
 495 * Z AND Y VALUES
 496 811310 0. 0.050300 0.051300 0.052600 0.051200 0.051400
 497 811311 0.051400 0.052400
 498 *
 499 801400 '2 EXTR. PRESS. DROP CONST. VS. THR. FLOW'
 500 * X VALUES
 501 811400 201000. 265000. 328500. 389000. 442000.
 502 811401 500500. 557000.
 503 * Z AND Y VALUES
 504 811410 0. 0.052900 0.056200 0.053700 0.049700 0.050200
 505 811411 0.052300 0.054900
 506 *
 507 801500 '1 EXTR. PRESS. DROP CONST. VS. TRH. FLOW'
 508 * X VALUES
 509 811500 201000. 265000. 328500. 389000. 442000.
 510 811501 500500. 557000.
 511 * Z AND Y VALUES
 512 811510 0. 0.053100 0.051200 0.056200 0.051400 0.052500
 513 811511 0.053200 0.052100
 514 *
 515 801900 '12-A BFP EFF. VS. PUMP FLOW'
 516 * X VALUES
 517 811900 8967. 112208. 134650. 157092. 179533.
 518 811901 201975. 224417. 246659. 269300. 291745.
 519 811902 314187. 336629. 359071. 381513. 403955.
 520 811903 426397. 448639.
 521 * Z AND Y VALUES
 522 811910 0. 0.476000 0.476000 0.456000 0.532000 0.572000

523 811911 0.610000 0.645000 0.675000 0.695000 0.713000
 524 811912 0.723000 0.730000 0.736000 0.730000 0.726000
 525 811913 0.722000 0.720000
 526 *
 527 802000 '12-A BFP HEAD VS. PUMP FLOW '
 528 * X VALUES
 529 812000 89767. 112208. 134650. 157092. 179533.
 530 812001 201975. 224417. 246858. 269300. 291745.
 531 812002 314187. 336629. 359071. 381513. 403955.
 532 812003 426397. 448839.
 533 * Z AND Y VALUES
 534 812010 0. 2394.000000 2380.000000 2373.000000 2363.000000
 535 + 2352.000000
 536 812011 2332.000000 2303.000000 2270.000000 2237.000000 2208.000000
 537 812012 2156.000000 2105.000000 2053.000000 1991.000000 1940.000000
 538 812013 1868.000000 1795.000000
 539 *
 540 802100 '12-B BFP EFF. VS. PUMP FLOW '
 541 * X VALUES
 542 812100 0. 22442. 44884. 67326. 89767.
 543 812101 112208. 134650. 157092. 179533. 201975.
 544 812102 224417. 246858. 269300. 291745. 314187.
 545 812103 336629. 359071. 381513. 403955. 426397.
 546 * Z AND Y VALUES
 547 812110 0. 0.000000 0.110000 0.205000 0.290000 0.370000
 548 812111 0.435000 0.495000 0.550000 0.595000 0.630000
 549 812112 0.660000 0.680000 0.700000 0.715000 0.725000
 550 812113 0.730000 0.738000 0.740000 0.742000 0.740000
 551 *
 552 802200 '12-B BFP HEAD VS. PUMP FLOW '
 553 * X VALUES
 554 812200 44883. 67325. 89767. 112208. 134650.
 555 812201 157092. 179533. 201975. 224417. 246858.
 556 812202 269300. 291745. 314187. 336629. 359071.
 557 812203 381513. 403955. 426397.
 558 * Z AND Y VALUES
 559 812210 0. 2404.000000 2394.000000 2390.000000 2383.000000
 560 + 2380.000000
 561 812211 2361.000000 2252.000000 2332.000000 2303.000000 2270.000000
 562 812212 2229.000000 2208.000000 2163.000000 2117.000000 2043.000000
 563 812213 1981.000000 1909.000000 1816.000000
 564 *
 565 ***** SCHEDULE VARIABLES
 566 *
 567 *
 568 *
 569 830100 1 BBHXGR 230 WW 5
 570 *
 571 *
 572 830200 2 BKELEI 1 BKGR0 1
 573 *
 574 *
 575 830300 3 EFFTRE 30 EQTFR 10
 576 *
 577 *
 578 830400 4 EFFTRE 50 EQTFR 10
 579 *
 580 *
 581 830500 5 EFFTRE 60 EQTFR 10
 582 *
 583 *
 584 830600 6 EFFTRE 140 EQTFR 10
 585 *
 586 *
 587 830700 7 EFFTRE 150 EQTFR 10
 588 *
 589 *
 590 830800 8 EFFTRE 160 EQTFR 10
 591 *
 592 *
 593 830900 9 EFFTRE 170 EQTFR 10
 594 *
 595 *
 596 831000 10 EFFTRE 180 EQTFR 10
 597 *
 598 *
 599 831100 11 PFAC1 54 WW 5
 600 *
 601 *
 602 831200 12 PFAC1 91 WW 5
 603 *
 604 *
 605 831300 13 PFAC1 154 WW 5
 606 *
 607 *
 608 831400 14 PFAC1 157 WW 5
 609 *
 610 *

611	831500	15	MFLBL1	431	WW	5
612	*					
613	*					
614	831900	19	EFFPMP	310	WW	313
615	*					
616	*					
617	832000	20	PMPDIS	310	WW	313
618	*					
619	*					
620	832100	21	EFFPMP	315	WW	317
621	*					
622	*					
623	832200	22	PMPDIS	315	WW	317
624	*					
625	***** OPERATIONAL VARIABLES					
626	*					
627	*					
628	870080	1000.				
629	*					
630	870330	3412.14				
631	*					
632	870980	100.				
633	*					
634	***** OPERATIONS					
635	*					
636	*					
637	880010	HH	5	SUB	HH	355
638	*					
639	880020	OPVB	10	MUL	WW	5
640	*					
641	880030	HH	115	SUB	HH	105
642	*					
643	880040	OPVB	12	MUL	WW	115
644	*					
645	880050	OPVB	11	ADD	OPVB	13
646	*					
647	880060	OPVB	14	DIV	BKGROS	1
648	*					
649	880070	OPVB	15	DIV	OPVB	9
650	*					
651	880080	OPVB	33	DIV	OPVB	16
652	*					
653	880090	OPVB	34	MUL	OPVB	98
654	*					
655	880100	HH	115	SUB	HH	165
656	*					
657	880110	PP	-165	PSH	SS	115
658	*					
659	880120	HH	115	SUB	OPVB	40
660	*					
661	880130	OPVB	39	DIV	OPVB	41
662	*					
663	880140	HH	165	SUB	HH	185
664	*					
665	880150	PP	-185	PSH	SS	165
666	*					
667	880160	HH	165	SUB	OPVB	44
668	*					
669	880170	OPVB	43	DIV	OPVB	45
670	*					
671	880180	EFFSEC	60	MUL	OPVB	98
672	*					
673	880190	OPVB	42	MUL	OPVB	98
674	*					
675	880200	OPVB	46	MUL	OPVB	98
676	*					
677	***** SPECIAL INPUT/OUTPUT					
678	*					
679	890010	'GROSS TURBINE CYCLE POWER OUTPUT	(MW)	,		
680	890011	BKGROS	0	,		
681	890020	'GROSS TURBINE CYCLE HEAT RATE	(BTU/KWH)	,		
682	890021	OPVB	16	,		
683	890030	'GROSS TURBINE CYCLE THERMAL EFFIC.	(%)	,		
684	890031	OPVB	35	,		
685	890040	'H.P. TURBINE SECTION EFFIC.	(%)	,		
686	890041	OPVB	36	,		
687	890050	'I.P. TURBINE SECTION EFFIC.	(%)	,		
688	890051	OPVB	37	,		
689	890060	'L.P. TURBINE SECTION EFFIC.	(%)	,		
690	890061	OPVB	38	,		
691	890070	'MAIN STEAM FLOW	(#/HR)	,		
692	890071	WW	5	,		
693	890080	'MAIN STEAM PRESSURE	(PSIA)	,		
694	890081	PP	9	,		
695	890090	'MAIN STEAM TEMPERATURE	(DEG-F)	,		
696	890091	TT	5	,		
697	890100	'1ST STAGE PRESSURE	(PSIA)	,		
698	890101	PP	5	,		

699	890110	'10TH STAGE PRESSURE	(PSIA)	'	
700	890111	PP	65		
701	890120	'COLD REHEAT PRESSURE	(PSIA)	'	
702	890121	PP	95		
703	890130	'COLD REHEAT TEMPERATURE	(DEG-F)	'	
704	890131	TT	95		
705	890140	'HOT REHEAT PRESSURE	(PSIA)	'	
706	890141	PP	115		
707	890150	'HOT REHEAT TEMPERATURE	(DEG-F)	'	
708	890151	TT	115		
709	890160	'I.P. INLET PRESSURE	(PSIA)	'	
710	890161	PP	136		
711	890170	'I.P. EXHAUST PRESSURE	(PSIA)	'	
712	890171	PP	165		
713	890180	'CONDENSER BACK PRESSURE	(IN-HG)	'	
714	890181	PP	195		
715	890190	'CIRC. WATER INLET TEMPERATURE	(DEG-F)	'	
716	890191	TT	932		
717	890200	'12-A BFP MOTOR POWER	,		
718	890201	BKPMOT	310	929.	I
719	890210	'12-B BFP MOTOR POWER	,		
720	890211	BKPMOT	315	895.	I
721	890220	'#6 FEEDWATER HEATER PRESSURE DROP	,		
722	890221	PDFW	350	12.	I
723	890230	'#5 FEEDWATER HEATER PRESSURE DROP	,		
724	890231	PDFW	340	7.9	I
725	890240	'#4 FEEDWATER HEATER PRESSURE DROP	,		
726	890241	PDFW	330		
727	890250	'#3 FEEDWATER HEATER PRESSURE DROP	,		
728	890251	PDFW	280	11.6	I
729	890260	'#2 FEEDWATER HEATER PRESSURE DROP	,		
730	890261	PDFW	270	14.4	I
731	890270	'#1 FEEDWATER HEATER PRESSURE DROP	,		
732	890271	PDFW	260	6.	I
733	*				
734	*				
735	*				
736	*				
737	*****				
738	*	END OF BASE DECK			
739	*****				
740	*				
741	*				
742	/				

LISTING OF INPUT DATA FOR CASE 2

```

1   *
2   = BEEBEE UNIT 12 - 12000 GAL/DAY MAKEUP
3   *
4   *
5   *
6   *****
7   *      GENERIC INPUT DATA
8   *****
9   *
10  * CYCLE FLAGS
11  010200  2    3    1    5    1    0    0.   0.   *** THIS CARD IS A REPLACEMENT CARD. ***
12  *
13  * PERSE OUTPUT SUPPRESSION CARDS
14  *
15  020000 NOPRNT PRINT
16  020003 PRINT
17  020006 PRINT
18  020007 PRINT
19  020008 PRINT
20  020009 PRINT
21  020010 PRINT
22  020020 PRINT
23  020023 PRINT
24  020038 PRINT
25  020039 PRINT
26  020040 PRINT
27  020076 PRINT
28  *
29  *
30  *****
31  *      SPECIAL STREAM SPECIFICATIONS
32  *****
33  *
34  ***** STREAM CLOSURES
35  *
36  * RADIAL SPILL STRIP LEAKAGE
37  601476 CLOSE
38  *
39  *
40  *****
41  *      COMPONENT DATA
42  *****
43  *
44  ***** CONDENSERS AND FEEDWATER HEATERS
45  *
46  * #3 Feedwater Heater
47  702800  17   1   150   3   0.   17.   *** THIS CARD IS A REPLACEMENT CARD. ***
48  702801  0.   0.   0.   0.   0.   0.   *** THIS CARD IS A REPLACEMENT CARD. ***
49  702802  0.   0.   0.   0.   0.   0.   0.   *** THIS CARD IS A REPLACEMENT CARD. ***
50  *
51  ***** SOURCES, SINKS, AND VALVES
52  *
53  * MAKE UP FLOW
54  700090  31   95.   15.   3750.   0.   0.   0
55  *
56  ***** SPLITTERS
57  *
58  * blowdown
59  703620  61   0.   3750.   *** THIS CARD IS A REPLACEMENT CARD. ***
60  *
61  *
62  *****
63  *      SPECIAL FEATURES
64  *****

```

65 *
 66 ***** SCHEDULES
 67 *
 68 *
 69 802100 '12-B BFP EFF. VS. PUMP FLOW

70 * X VALUES
 71 812100 0. 22442. 44884. 67326. 89767.
 72 812101 112208. 134650. 157092. 179533. 201975.
 73 812102 224417. 246859. 269300. 291745. 314187.
 74 812103 336629. 359071. 381513. 403955. 426397.
 75 * Z AND Y VALUES
 76 812110 0. 0.000000 0.110000 0.205000 0.290000 0.370000
 77 812111 0.435000 0.495000 0.550000 0.595000 0.630000
 78 812112 0.660000 0.680000 0.700000 0.715000 0.725000
 79 812113 0.730000 0.738000 0.740000 0.742000 0.740000
 80 *
 81 802200 '12-B BFP HEAD VS. PUMP FLOW

82 * X VALUES
 83 812200 44883. 67325. 89767. 112208. 134650.
 84 812201 157092. 179533. 201975. 224417. 246859.
 85 812202 269300. 291745. 314187. 336629. 359071.
 86 812203 381513. 403955. 426397.
 87 * Z AND Y VALUES
 88 812210 0. 2404.000000 2394.000000 2390.000000 2383.000000
 89 + 2380.000000

90 812211 2361.000000 2252.000000 2332.000000 2303.000000 2270.000000
 91 812212 2229.000000 2208.000000 2163.000000 2117.000000 2043.000000
 92 812213 1981.000000 1909.000000 1816.000000

93 *
 94 ***** SCHEDULE VARIABLES
 95 *
 96 *
 97 *
 98 830300 3 EFFTRE 30 EQTFR 10 *** THIS CARD IS A REPLACEMENT CARD. ***
 99 830303 DELETE
 100 *
 101 *
 102 830400 4 EFFTRE 50 EQTFR 10 *** THIS CARD IS A REPLACEMENT CARD. ***
 103 830403 DELETE
 104 *
 105 *
 106 830500 5 EFFTRE 60 EQTFR 10 *** THIS CARD IS A REPLACEMENT CARD. ***
 107 830503 DELETE
 108 *
 109 *
 110 830600 6 EFFTRE 140 EQTFR 10 *** THIS CARD IS A REPLACEMENT CARD. ***
 111 830603 DELETE
 112 *
 113 *
 114 830700 7 EFFTRE 150 EQTFR 10 *** THIS CARD IS A REPLACEMENT CARD. ***
 115 830703 DELETE
 116 *
 117 *
 118 830800 8 EFFTRE 160 EQTFR 10 *** THIS CARD IS A REPLACEMENT CARD. ***
 119 830803 DELETE
 120 *
 121 *
 122 830900 9 EFFTRE 170 EQTFR 10 *** THIS CARD IS A REPLACEMENT CARD. ***
 123 830903 DELETE
 124 *
 125 *
 126 831000 10 EFFTRE 180 EQTFR 10 *** THIS CARD IS A REPLACEMENT CARD. ***

127 831008 DELETE
128 *
129 *
130 831100 11 PFAC1 54 WW 5 *** THIS CARD IS A REPLACEMENT CARD. ***
131 831108 DELETE
132 *
133 *
134 831200 12 PFAC1 91 WW 5 *** THIS CARD IS A REPLACEMENT CARD. ***
135 831208 DELETE
136 *
137 *
138 831300 13 PFAC1 154 WW 5 *** THIS CARD IS A REPLACEMENT CARD. ***
139 831308 DELETE
140 *
141 *
142 831400 14 PFAC1 157 WW 5 *** THIS CARD IS A REPLACEMENT CARD. ***
143 831408 DELETE
144 *
145 *
146 831500 15 PFAC1 431 WW 5 *** THIS CARD IS A REPLACEMENT CARD. ***
147 831508 DELETE
148 *
149 *
150 831608 DELETE
151 *
152 *
153 831708 DELETE
154 *
155 *
156 831808 DELETE
157 *
158 *
159 831900 19 EFFFMP 310 WW 313 *** THIS CARD IS A REPLACEMENT CARD. ***
160 831908 DELETE
161 *
162 *
163 832000 20 PMPDIS 310 WW 313 *** THIS CARD IS A REPLACEMENT CARD. ***
164 832008 DELETE
165 *
166 *
167 832100 21 EFFFMP 315 WW 317 *** THIS CARD IS A REPLACEMENT CARD. ***
168 832108 DELETE
169 *
170 *
171 832200 22 PMPDIS 315 WW 317 *** THIS CARD IS A REPLACEMENT CARD. ***
172 832208 DELETE
173 *
174 *
175 .

APPENDIX C

SPECIAL OUTPUT TABLE OF SPECIFIED VARIABLES

INDEX	DESCRIPTION	VARIABLE (ID)	VALUE
1	GROSS TURBINE CYCLE POWER OUTPUT (MW)	BKGROS(0)	83.4238
2	GROSS TURBINE CYCLE HEAT RATE (BTU/KWH)	CPVB (16)	7820.4954
3	GROSS TURBINE CYCLE THERMAL EFFIC. (%)	CPVB (35)	43.6307
4	H.P. TURBINE SECTION EFFIC. (%)	CPVB (36)	83.6026
5	I.P. TURBINE SECTION EFFIC. (%)	CPVB (37)	89.0880
6	L.P. TURBINE SECTION EFFIC. (%)	CPVB (38)	76.0570
7	MAIN STEAM FLOW (#/HR)	WW (5)	557000.0000
8	MAIN STEAM PRESSURE (PSIA)	PP (5)	1815.0000
9	MAIN STEAM TEMPERATURE (DEG-F)	TT (5)	1050.0000
10	1ST STAGE PRESSURE (PSIA)	PP (35)	1486.6454
11	10TH STAGE PRESSURE (PSIA)	PP (65)	357.5645
12	COLD REHEAT PRESSURE (PSIA)	PP (95)	357.5645
13	COLD REHEAT TEMPERATURE (DEG-F)	TT (95)	649.7359
14	HOT REHEAT PRESSURE (PSIA)	PP (115)	321.8438
15	HOT REHEAT TEMPERATURE (DEG-F)	TT (115)	1000.0000
16	I.P. INLET PRESSURE (PSIA)	PP (136)	315.4069
17	I.P. EXHAUST PRESSURE (PSIA)	PP (165)	18.4280
18	CONDENSER BACK PRESSURE (IN-HG)	PP (195)	0.4941
19	CIRC. WATER INLET TEMPERATURE (DEG-F)	TT (932)	54.0000
24	#4 FEEDWATER HEATER PRESSURE DROP	PDFW (330)	0.0000

SPECIAL OUTPUT TABLE OF SPECIFIED VARIABLES

INDEX	DESCRIPTION	VARIABLE (ID)	VALUE
1	GROSS TURBINE CYCLE POWER OUTPUT (MW)	BKGROS(0)	83.3520
2	GROSS TURBINE CYCLE HEAT RATE (BTU/KWH)	CPVB (16)	7826.9764
3	GROSS TURBINE CYCLE THERMAL EFFIC. (%)	CPVB (35)	43.5946
4	H.P. TURBINE SECTION EFFIC. (%)	CPVB (36)	83.6040
5	I.P. TURBINE SECTION EFFIC. (%)	CPVB (37)	89.0898
6	L.P. TURBINE SECTION EFFIC. (%)	CPVB (38)	76.0598
7	MAIN STEAM FLOW (#/HR)	WW (5)	557000.0000
8	MAIN STEAM PRESSURE (PSIA)	PP (5)	1815.0000
9	MAIN STEAM TEMPERATURE (DEG-F)	TT (5)	1050.0000
10	1ST STAGE PRESSURE (PSIA)	PP (35)	1486.6439
11	10TH STAGE PRESSURE (PSIA)	PP (65)	357.3300
12	COLD REHEAT PRESSURE (PSIA)	PP (95)	357.3300
13	COLD REHEAT TEMPERATURE (DEG-F)	TT (95)	649.5953
14	HOT REHEAT PRESSURE (PSIA)	PP (115)	321.6328
15	HOT REHEAT TEMPERATURE (DEG-F)	TT (115)	1000.0000
16	I.P. INLET PRESSURE (PSIA)	PP (136)	315.2001
17	I.P. EXHAUST PRESSURE (PSIA)	PP (165)	18.4280
18	CONDENSER BACK PRESSURE (IN-HG)	PP (195)	0.4945
19	CIRC. WATER INLET TEMPERATURE (DEG-F)	TT (932)	54.0000
24	#4 FEEDWATER HEATER PRESSURE DROP	PDFW (330)	0.0000

SPECIAL OUTPUT TABLE OF SPECIFIED VARIABLES

INDEX	DESCRIPTION	VARIABLE (ID)	VALUE
1	GROSS TURBINE CYCLE POWER OUTPUT (MW)	BKGROS(0)	83.3132
2	GROSS TURBINE CYCLE HEAT RATE (BTU/KWH)	GPVB (16)	7830.5634
3	GROSS TURBINE CYCLE THERMAL EFFIC. (%)	GPVB (35)	43.5746
4	H.P. TURBINE SECTION EFFIC. (%)	GPVB (36)	83.6043
5	I.P. TURBINE SECTION EFFIC. (%)	GPVB (37)	89.0898
6	L.P. TURBINE SECTION EFFIC. (%)	GPVB (38)	76.0567
7	MAIN STEAM FLOW (#/HR)	WW (5)	557000.0000
8	MAIN STEAM PRESSURE (PSIA)	PP (5)	1815.0000
9	MAIN STEAM TEMPERATURE (DEG-F)	TT (5)	1050.0000
10	1ST STAGE PRESSURE (PSIA)	PP (35)	1486.6439
11	10TH STAGE PRESSURE (PSIA)	PP (65)	357.2693
12	COLD REHEAT PRESSURE (PSIA)	PP (95)	357.2693
13	COLD REHEAT TEMPERATURE (DEG-F)	TT (95)	649.5593
14	HOT REHEAT PRESSURE (PSIA)	PP (115)	321.5781
15	HOT REHEAT TEMPERATURE (DEG-F)	TT (115)	1000.0000
16	I.P. INLET PRESSURE (PSIA)	PP (136)	315.1465
17	I.P. EXHAUST PRESSURE (PSIA)	PP (165)	18.4280
18	CONDENSER BACK PRESSURE (IN-HG)	PP (195)	0.4946
19	CIRC. WATER INLET TEMPERATURE (DEG-F)	TT (932)	54.0000
24	#4 FEEDWATER HEATER PRESSURE DROP	PDFW (330)	0.0000

PEPSI CODE BY HALLIBURTON NUS, IDAHO FALLS, ID. VERSION 570 CREATED 10 SEP 92
BEEBEE UNIT 12 - 28 TUBES PLUGGED. 1900 #/HR LEAK #3-#2 HTR

DATE 02/26/93.

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SPECIAL OUTPUT TABLE OF SPECIFIED VARIABLES

INDEX	DESCRIPTION	VARIABLE (ID)	VALUE
1	GROSS TURBINE CYCLE POWER OUTPUT (MW)	BKGROS(0)	83.2910
2	GROSS TURBINE CYCLE HEAT RATE (BTU/KWH)	GPVB (16)	7832.5467
3	GROSS TURBINE CYCLE THERMAL EFFIC. (%)	GPVB (35)	43.5631
4	H.P. TURBINE SECTION EFFIC. (%)	GPVB (36)	83.6043
5	I.P. TURBINE SECTION EFFIC. (%)	GPVB (37)	89.0893
6	L.P. TURBINE SECTION EFFIC. (%)	GPVB (38)	76.0551
7	MAIN STEAM FLOW (#/HR)	WW (5)	557000.0000
8	MAIN STEAM PRESSURE (PSIA)	PP (5)	1815.0000
9	MAIN STEAM TEMPERATURE (DEG-F)	TT (5)	1050.0000
10	1ST STAGE PRESSURE (PSIA)	PP (35)	1486.6439
11	10TH STAGE PRESSURE (PSIA)	PP (65)	357.2656
12	COLD REHEAT PRESSURE (PSIA)	PP (95)	357.2656
13	COLD REHEAT TEMPERATURE (DEG-F)	TT (95)	649.5571
14	HOT REHEAT PRESSURE (PSIA)	PP (115)	321.5748
15	HOT REHEAT TEMPERATURE (DEG-F)	TT (115)	1000.0000
16	I.P. INLET PRESSURE (PSIA)	PP (136)	315.1433
17	I.P. EXHAUST PRESSURE (PSIA)	PP (165)	18.4280
18	CONDENSER BACK PRESSURE (IN-HG)	PP (195)	0.4947
19	CIRC. WATER INLET TEMPERATURE (DEG-F)	TT (932)	54.0000
24	#4 FEEDWATER HEATER PRESSURE DROP	PDFW (330)	0.0000