

**Replacing Defective Feedwater Heaters  
With Spares From A Steam To Combined Cycle Repowering**

**Michael J. Barrios, P.E.**

**Florida Power & Light Company**

**REPLACING DEFECTIVE FEEDWATER HEATERS WITH  
SPARES FROM A STEAM TO COMBINED CYCLE REPOWERING**

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Florida Power & Light Company**

The Fort Lauderdale Plant is scheduled to be repowered to a combined cycle unit starting in the Fall of 1992. The existing unit is a gas/oil-fired 137 MW, 1450 psig reheat unit with a Westinghouse turbine and a Babcox & Wilcox (B & W) boiler. The unit became commercial in 1957. The existing unit has six feedwater heaters, two high pressure and four low pressure. The repowered unit will use the existing steam turbine and the two LP neck feedwater heaters. Attachment 1 is a heat balance of the existing unit and Attachment 2 is a heat balance of the repowered unit. The number 6 feedwater heater or 13th stage heater on Unit 4 was replaced in 1978. FPL has plans to use this heater to replace an out-of-service feedwater heater at the Cutler Plant Unit 5 (PCU5).

The Cutler Unit 5 is a 67 MW gas-fired 1350 psig non-reheat unit with a Westinghouse turbine and a Combustion Engineering (CE) boiler. The unit became commercial in 1954. A heat balance for the Cutler 5 unit can be seen in Attachment 3. The number 5 feedwater heater or 11th stage heater has been bypassed and removed from service due to excessive plugging and a high failure rate.

A PEPSE study was performed to determine how the Fort Lauderdale Unit 4 (PFL4), number 5 feedwater heater would perform on the Cutler unit. The Engineering Department determined that PFL4 heater physically would fit on the PCU5 unit.

The first step in the study was to build a feedwater heater submodel to match the feedwater manufacturer's design specification sheet. A simplified feedwater heater design model was build for the heater. The heat transfer coefficient ( $u$ ) of the sections and the baffle spacings were varied to meet the design conditions for the heater. This was necessary since there were no drawings of the heater's internal configuration. The feedwater outlet and the drain outlet pressure and temperature were used to validate the model against the manufacturer's specification sheet. The PFL4 acceptance data also was entered into the feedwater heater submodel for further validation. The model's results using the acceptance test data did not agree as closely as the data from the manufacturer's specification sheet, but at acceptance the unit had a different heater. The feedwater heater outlets were within 1°F of the acceptance data so we felt that the submodel was an accurate model of the existing feedwater heater.

The next step was to build the turbine cycle model for the Cutler 5 unit. This unit is a peaking unit that only operates during periods of high demand. The PEPSE turbine cycle model was built and verified against the unit's VWO heat balance. The number 5 feedwater heater was modeled in the performance mode to match the VWO heat balance. The simplified design mode submodel was incorporated into the turbine cycle model to perform the sensitivity studies. The inlet drain of the submodel had to be eliminated since this heater would be the last heater in the train at PCU5.

There were four operating scenarios that FPL wanted to analyze. They were (1) Installing the heater with no modification to the feedwater heater, (2) Plugging tubes to match the feedwater design tube velocity, (3) Throttling extraction flow to match original heat balance generation, and (4) Installing a flow restricting orifice in the extraction line to maintain the original extraction flow.

Table 1 is a summary of the first three scenarios. The flow restricting orifice was ruled out because the critical orifice ID would have been 1.6 inches and we did not

want to risk plugging the throat during long reserve shutdown periods. The extraction pipe is six inch schedule 40.

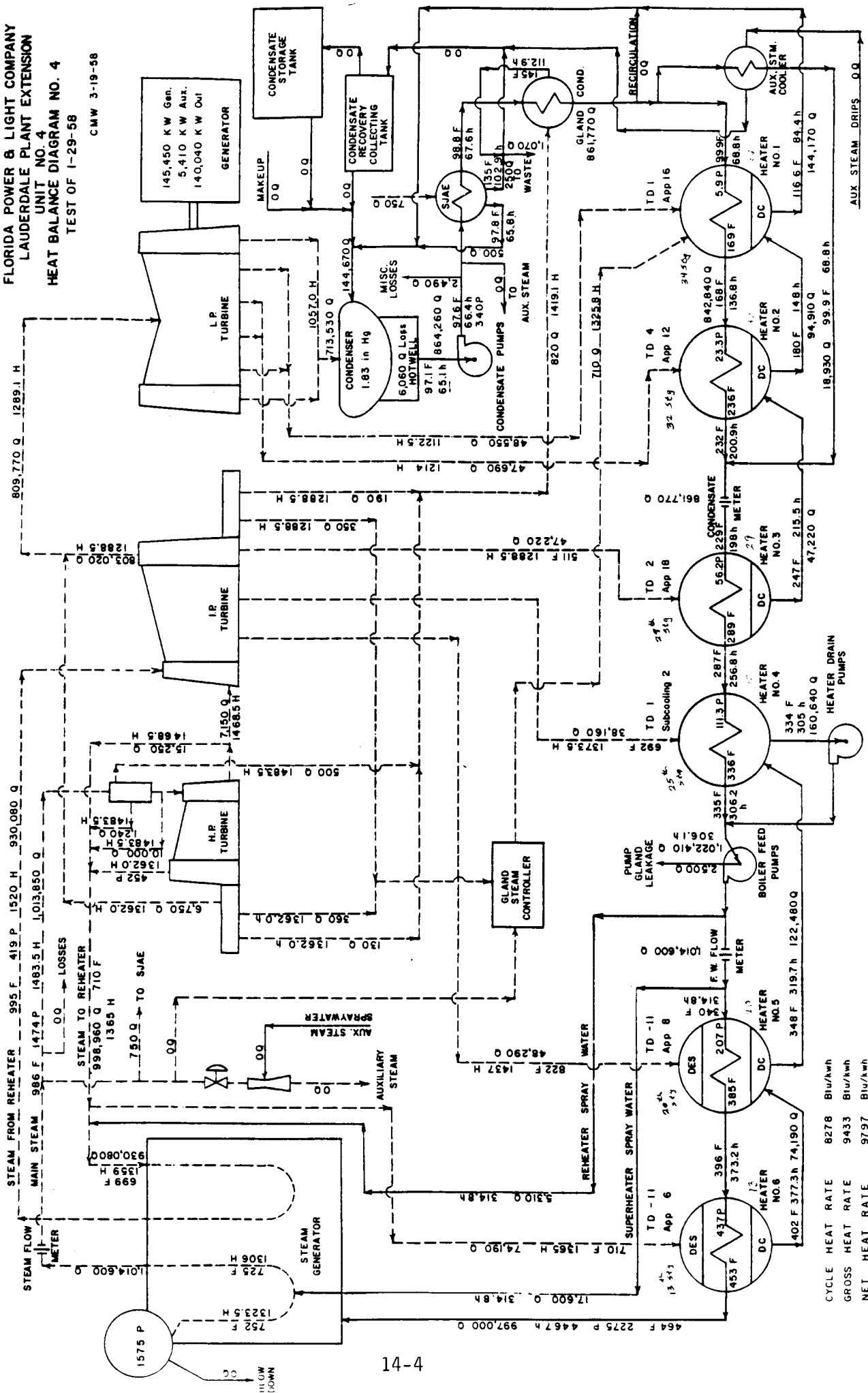
In conclusion, we determined that throttling the extraction flow to regain lost generation would be the best operating mode. The Cutler Plant will save about \$300,000 by using the feedwater heater from the Fort Lauderdale Unit 4 instead of purchasing a new heater.

TABLE 1

<u>SCENARIO</u>	<u>FW IN °F</u>	<u>FW OUT °F</u>	<u>STEAM IN °F</u>	<u>DRAIN OUT°F</u>	<u>GROSS GEN MW</u>	<u>TCHR BTU/KWH</u>
PCU 5 Original Heat Balance	355	423.5	654.8	375.0	74.6	9102
PCU5 with PFL4 Heater w/no Modification	355	442.1	654.8	359.3	73.6	9059
117 Plugged Tubes to Match Design FWH Tube Velocity (Design Velocity = 7.4 ft/sec)	355	439.7	654.8	364.4	73.7	9065
PCU5 with PFL4 Heater and Throttling of Extraction Flow to Match Original Heat Balance Generation	355	423.8	647.2	356.4	74.6	

FLORIDA POWER & LIGHT COMPANY  
LAUDERDALE PLANT EXTENSION  
UNIT NO. 4  
HEAT BALANCE DIAGRAM NO. 4  
TEST OF 1-29-58

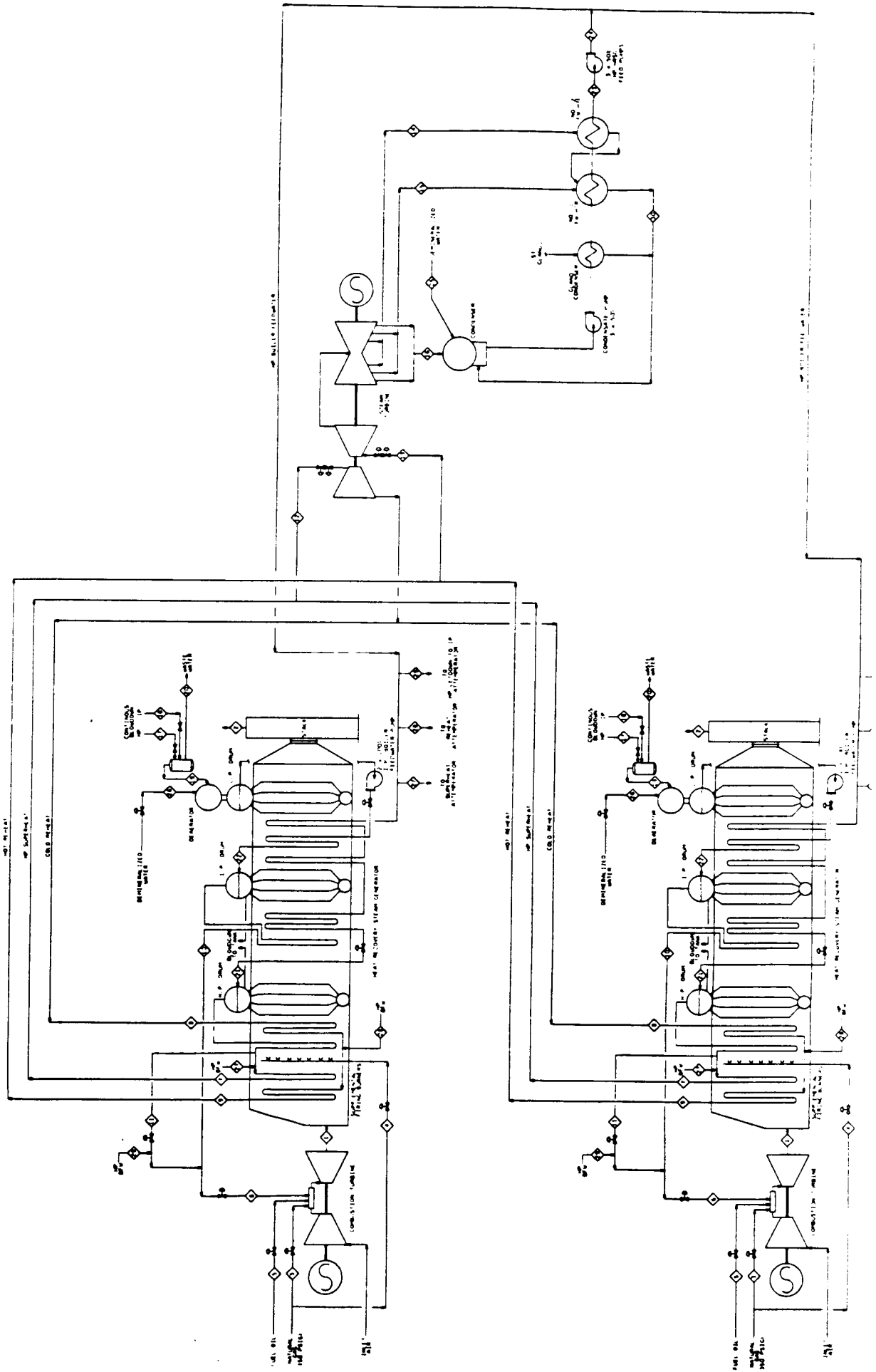
CMW 3-19-58



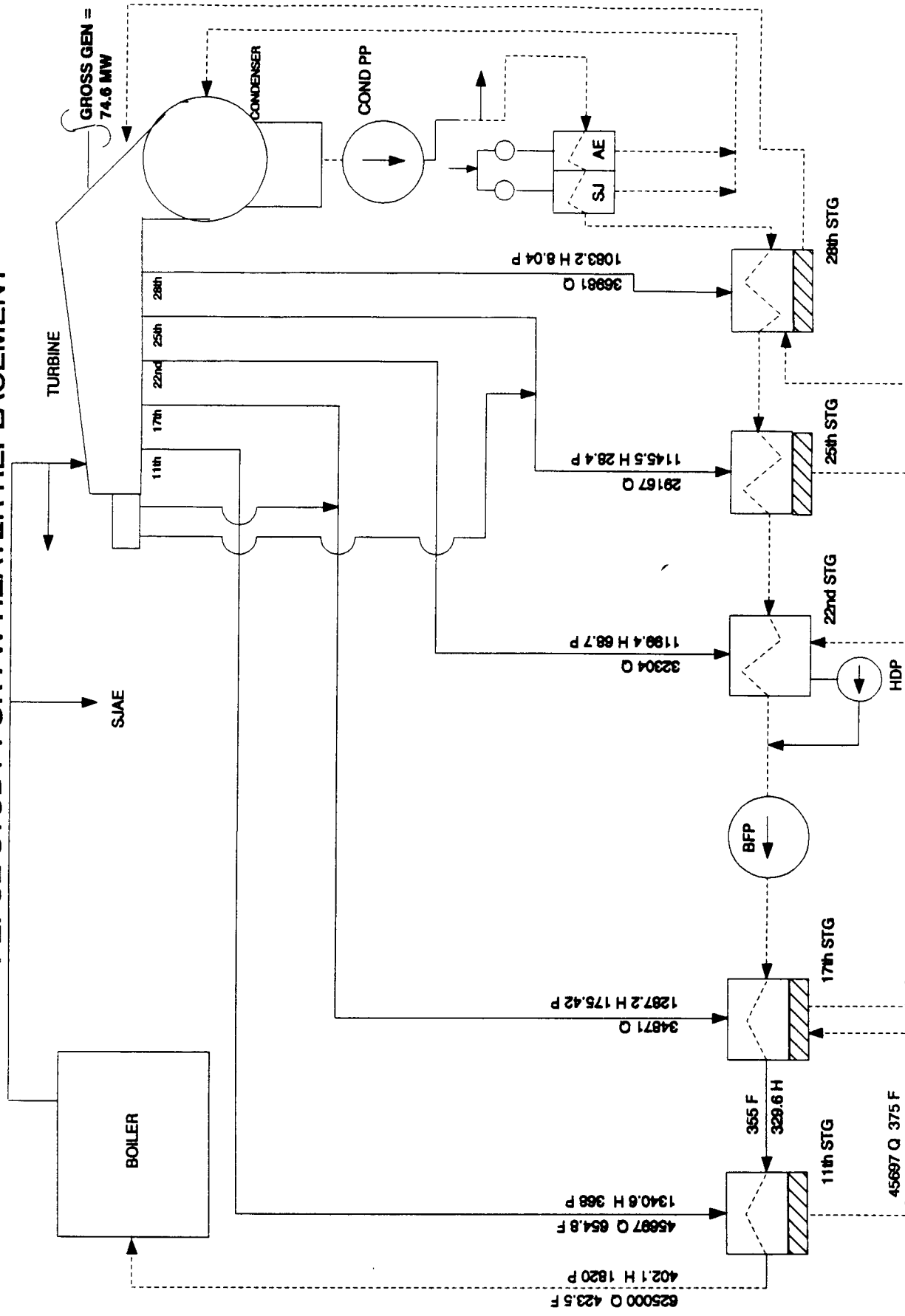
CYCLE HEAT RATE	8278	Blu/kwh
GROSS HEAT RATE	9433	Blu/kwh
NET HEAT RATE	9797	Blu/kwh
BOILER EFFICIENCY	87.75	%

ATTACHMENT I

# FLORIDA POWER & LIGHT LAUDERDAL PLANT UNITS 4 & 5 COMBUSTION TURBINE REPOWERING



# PEPSE STUDY FOR FW HEATER REPLACEMENT



NET TCHR = 9102 BTU/KWH

PRS/TS/MAJB

PCU5 HEAT BALANCE WITH ORIGINAL HEATER

```

= DESIGN MODE HEATER FOR PCU5 STUDY
*
* THIS IS A FW HTR SUB MODEL FOR PFL 4 HTR 5 TO GO
* TO PCU 5 HTR 5.
* BY M.J. BARRIOS 2/4/91
* DEBUG
010200 3 0 0 0 0 0 0.0 * DEBUGOFF=0 WORD 6
01200010 0 0 0 0 0 2 * SET ITERMIN TO 2
506000 610, U, 620, I
506100 620, U, 630, I
506200 620, B, 640, S
506300 660, U, 640, I
506400 640, T, 650, I
506600 640, D, 680, I
*
* DRAIN STREAM
506500 700, U, 640, D
*
*
* TEMP PRESS FLOW
*706100 33, 795.9 218.0 1.0E07 *HEATER DESING SPEC SHEET
*706100 33, 822.0 207.0 1.0E07 *PFL4 ACC TEST DATA
706100 33, 656.0 368.0 1.0E07 * PCU 5 HEAT BALANCE
706200 60 0.0 44400.0
706300 32
706500 30
706800 30
*
* TEMP PRESS FEEDWATER FLOW
*706600 31 333.0 2260.0 1010750. * DESIGN SPEC DATA
*706600 31 340.0 2260.0 997000.0 * PFL 4 ACC TEST DATA
706600 31 357.0 1815.0 625000. * PCU 5 HEAT BALANCE
*
* DRAIN INLET FLOW
*707000 31 408.1 437. 79920.0 *DESIGN SPEC SHEET
*707000 31 402.0 437. 74190.0 * PFL 4 ACC TESTET
707000 31 402.0 437. 0.0 * PCU 5 HEAT BALANCE

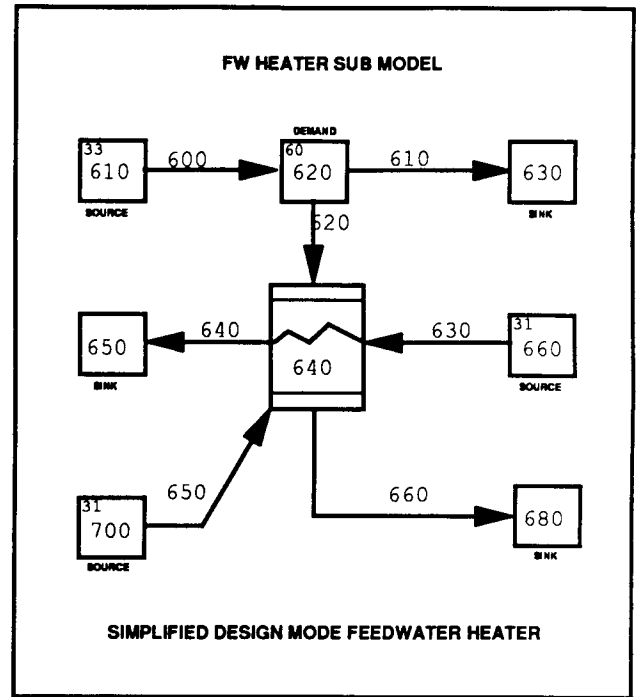
```

DESIGN MODE HEATER DATA

```

*
*
* 1 2! 3 4 5
* CTYPE !DRAIN IDXTGE NMODFW FRFWUT
706400 18 1 -620 4 0.0
*
* 6 7 8 9 10
* IGFLC IFFLC IFLDFC IFLGCR HTRORT
*706400 2 2 0 0 1
*
* 11 12 13 14
* IGFLDS IFFLDS IGFLDC IFFLDC
*706400 2 2 2 2
*
* CONDENSING SECTION DATA THERM COND.
* 1 2 3 4 5 6
* DIDC DODC XLC XNC !XKTC! SLC
706401 .527 .625 720. 402. 45. .8125
*
* 7 8 9! 10
* DNZFWI DNZFWO DNZI DNZO
706402 10.0 10.0 11.66 6.0
*
* U VALU PITCH LEVEL
706403 0.0 0.0 0.0 795. .8125 5.0
*
* DESUPERHEATING SECTION
* 1 2 3
* XLDS ?SEFLDS? XBFLDS
706404 87.0 200. 4.
*
* BAFFLE #
706405 0.0 1.0 1.0 0.0 0.0 113. * U VALUE
*
* DRAIN COOLER SECTION
* 1 2 3
* XLDC ?SBFLDC? XBFLDC
706406 72.0 200. 7.
*
* BAFFLE #
706407 0.0 1.0 1.0 0.0 0.0 489. * U VALUE

```





**FEEOWATER HEATER SPECIFICATION SHEET** Rev. 2: 3-10-78  
 Rev. 1: 2-23-78

<b>CUSTOMER</b> Florida Power & Light Company	<b>JOB NO.</b> 6056-10
<b>STATION</b> Ft. Lauderdale Plant	<b>FILE NO.</b> 30010
<b>PLANT LOCATION</b> Florida	<b>UNIT NO.</b> 5
<b>SERVICE OF UNIT</b> H. P. Heater #5	<b>INQUIRY NO.</b> TWS 241805
<b>SIZE:</b> 37.5 - 357	<b>DATE</b> 9/16/77
<b>TYPE:</b> Horizontal U-Tube	<b>ITEM NO.</b> 2
<b>SURFACE/SHELL</b> 3938	<b>NO. OF UNITS</b> 1
<b>EFF. SQ. FT.</b> 3999	<b>SHELLS/UNIT</b> 1
<b>CROSS SQ. FT.</b> 3938	<b>EFF. SQ. FT.</b> 3999
<b>CROSS SQ. FT.</b>	<b>CROSS SQ. FT.</b>

**PERFORMANCE OF ONE UNIT**

FLUID CIRCULATED	SHELL SIDE		TUBE SIDE
	STEAM	DRAINS	FEED WATER
TOTAL FLUID ENTERING	52,355	79,920	1,010,750
INLET ENTHALPY	1422	383.9	307.0
OUTLET ENTHALPY	319.8	319.8	369.2
INLET TEMPERATURE	795.9 (389.1 SAT.)	408.1	333
OUTLET TEMPERATURE	348.2		392.6
OPERATING PRESSURE	218		2000
NUMBER OF PASSES PER SHELL	3 ZONES		2
VELOCITY	FT./SEC.		7.4 AT 60°F.
PRESSURE DROP	(A) 1.7	(C) 3.9	12.3

	HEAT EXCHANGED BTU/HR.	MTD °F	TRANSFER RATE BTU/HR/SQ FT/°F	SURFACE EFF SQ FT	BAFFLE SPACING	THK.	NUMBER
(A) DESUPERHEATING SECTION	9,750,000	182.9	113	473	17.4	.625	5
(B) CONDENSING SECTION	47,430,000	19.4	795	3068	34.6	.625	8
(C) DRAIN COOLING SECTION	5,670,000	29.2	489	397	6.9	.375	9

**CONSTRUCTION OF EACH SHELL**

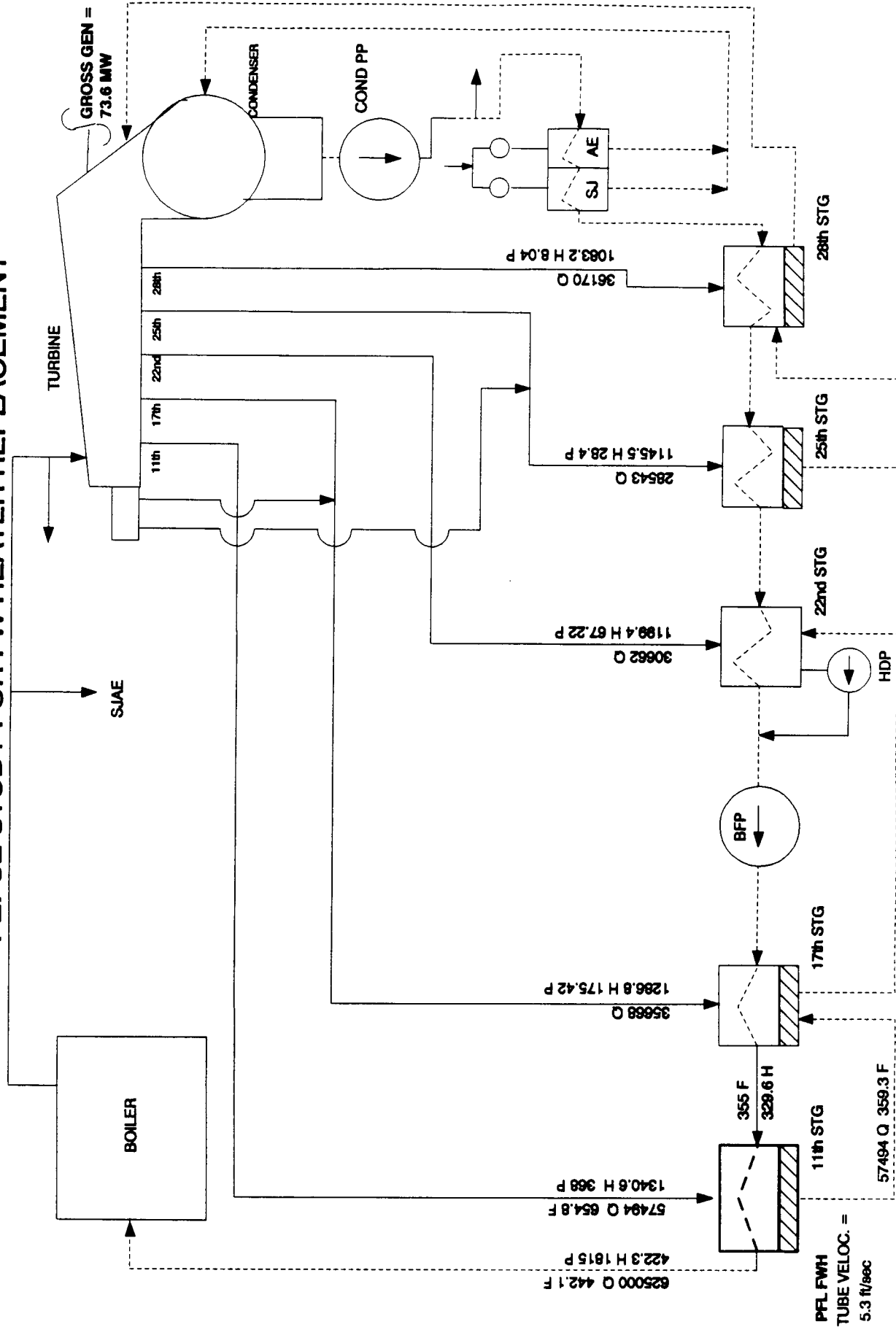
DESIGN PRESSURE	PSIG	300		2600
TEST PRESSURE	PSIG	450		3900
DESIGN TEMPERATURE	°F	STM BOX 850	SKIRT 650	SHELL 650
CONNECTIONS: SIZE		IN 10	OUT 6	IN 10
TYPE		BW: 300# Flg.		BW Sch. 160
TUBES: NO. 402U	O.D. 5/8"	BWG 18	NO. AVG. LENGTH 357"	STR. PITCH 13/16"
DEBUP SHROUD LENGTH 87"		DR CLS SHROUD TYPE	Full Pass	LENGTH 73"
CONSTRUCTION—ASME SECTION VIII DIVISION I		1974	HEI STDS. Yes	CUST. SPEC.
WEIGHTS: EMPTY 27,100		FULL OF WATER 41,000	REMOVABLE SHELL/RINGER	6600

PART	MATERIAL	THK.	CORR. ALLOW.	GASKETS	MATERIAL
TUBES NI-CU	SB163	DER .049	-	Shell - Skirt	Flexitallic $\Delta$
FIXED T.B.	SA266-II	5.5			
SHELL 37 1/2" ID	SA515-70	7/16		TUBE TO TUBE SHEET JOINT	Welded & Rolled
SHELL COVER F-D	SA515-70	.563		TUBE SHEET OVERLAY	Monel
TUBE SUPPORTS 8	SA283-C	5/8		TYPE OF SHELL SUPPORTS	Fixed
CROSS BAFFLES 5, 9	SA283-C	5/8 & 3/8		SHELL TO SKIRT JOINT	Flanged
CHANNEL	SA266-II	5.1875		TYPE OF CHAN. AND CLOSURE	Breechlock
CHANNEL COVER	SA266-II	8.5			
SHROUD	SA-283-C	1/4		INTERIOR CORR. CONTROL PROCEDURE	
IMPINGEMENT BAFFLE	SA240Tp304	1/4		NUMBER OF TUBES (LINE 27) INCLUDES	2 INSTALLED SPARES
Steam Box	SA387-II CL.1	1/4			

SHELL SAFETY VALVE: MANUF.	--	MODEL NO.
TUBESIDE RELIEF VALVE: MANUF.	--	MODEL NO.
OTHER ACCESSORIES:	Insulation Clips	



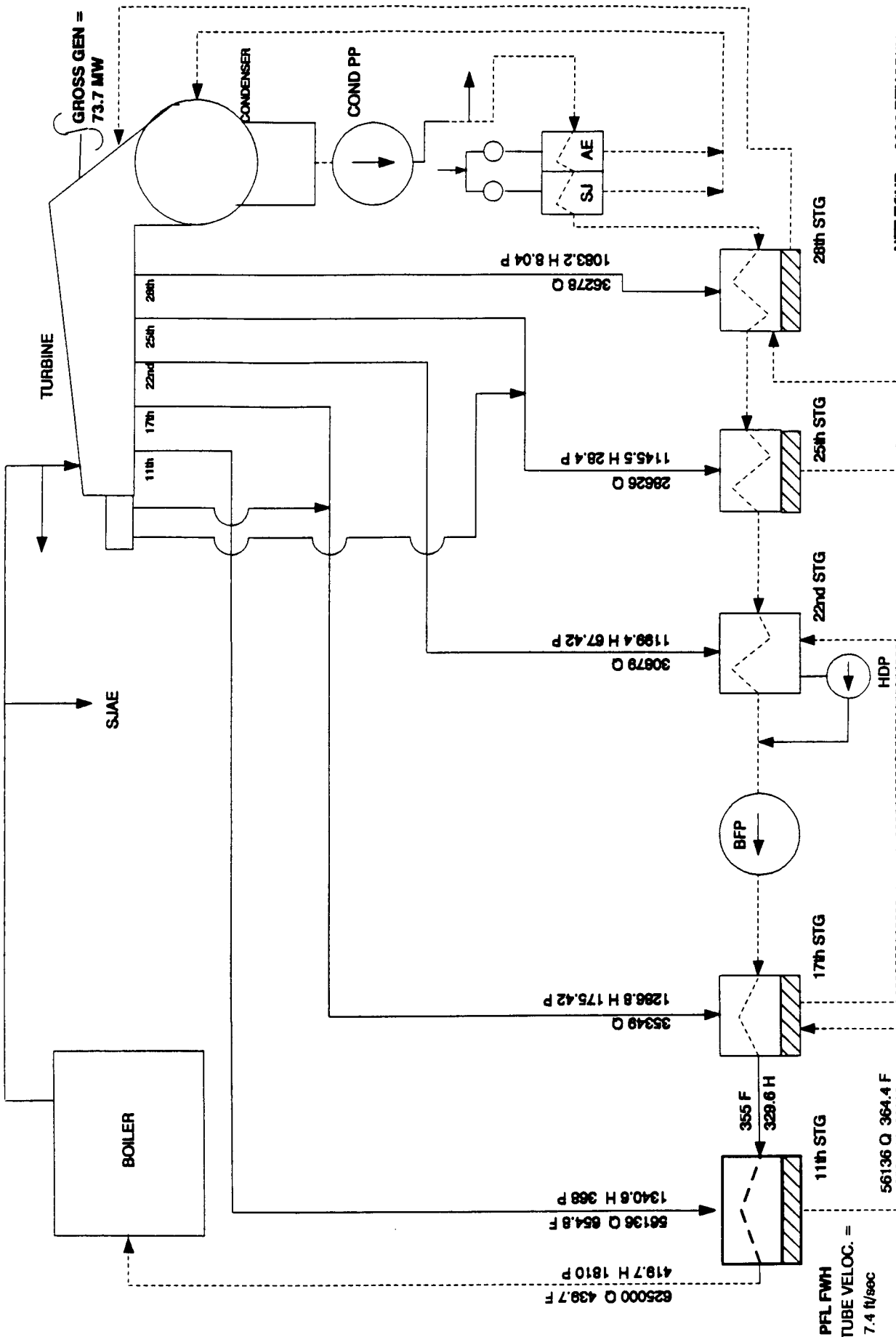
# PEPSE STUDY FOR FW HEATER REPLACEMENT



**PCU5 HEAT BALANCE WITH PFL4 FWH  
W/O ANY MODIFICATIONS**

PRS/TS/MJB

# PEPSE STUDY FOR FW HEATER REPLACEMENT



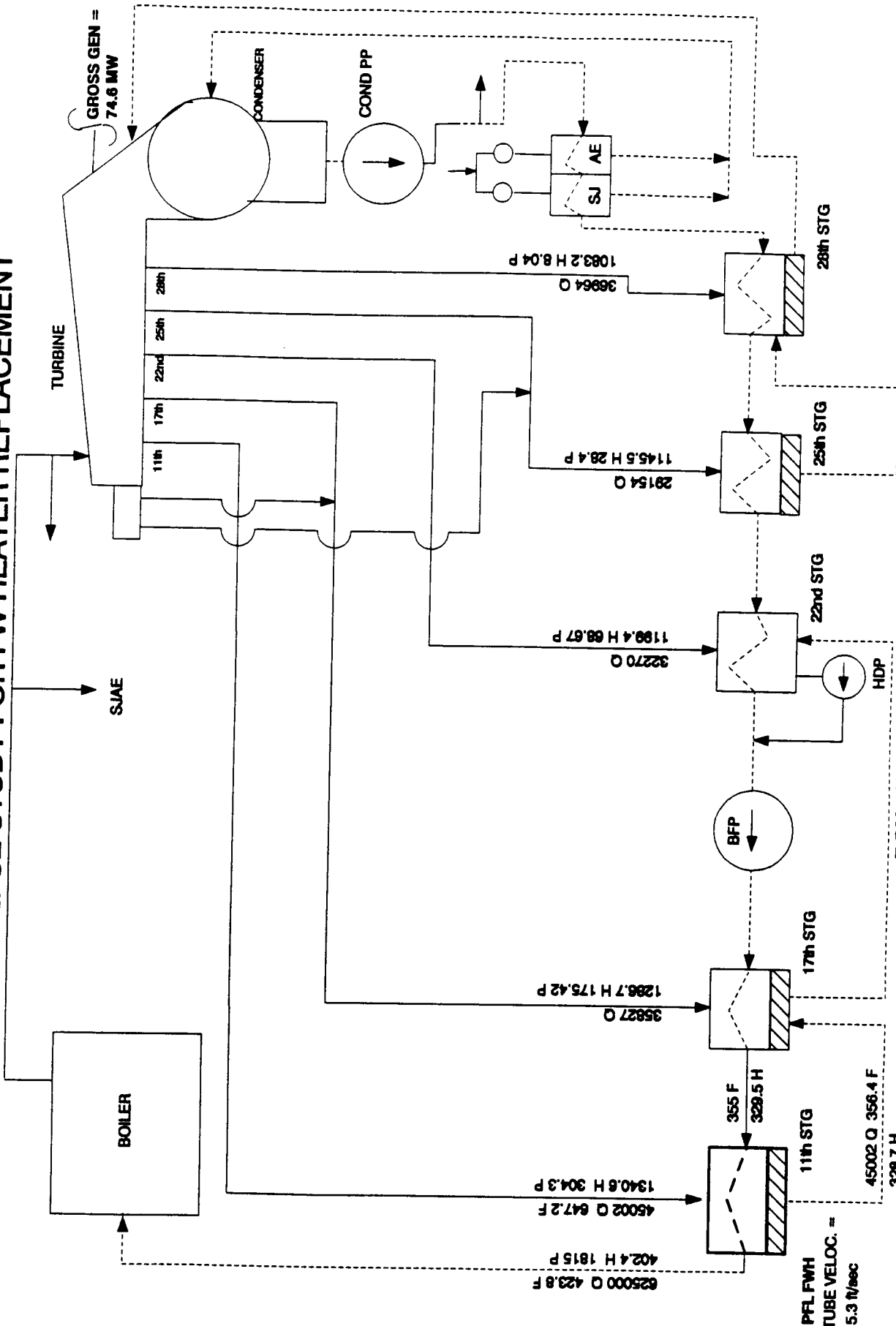
NET TCHR = 9065 BTU/KWH

PRS/TSMJIB

**PCU5 HEAT BALANCE WITH PFL4 FW HEATER AND 117 TUBES PLUGGED.**

PFL FW HEAT BALANCE WITH PFL4 FW HEATER AND 117 TUBES PLUGGED.  
TUBE VELOC. = 7.4 ft/sec

# PEPSE STUDY FOR FW HEATER REPLACEMENT



NET TCHR = 9100 BTU/KWH  
 PRS/TS/MAJB  
**PCU5 HEAT BALANCE WITH PFL4 FWHT  
 THROTTLING OF EXTRACTION FLOW  
 TO MATCH ORIGINAL HEAT BAL. GENERATION**

```

= DESIGN MODE HEATER FOR PCU5 STUDY
*
* THIS IS A FW HTR SUB MODEL FOR PFL 4 HTR 5 TO GO
* TO PCU 5 HTR 5.
* BY M.J. BARRIOS 2/4/91
*
*          DEBUG
010200 3 0 0 0 0 0 0.0 * DEBUGOFF=0 WORD 6
01200010 0 0 0 0 0 2 * SET ITERMIN TO 2
506000 610, U, 620, I
506100 620, U, 630, I
506200 620, B, 640, S
506300 660, U, 640, T
506400 640, T, 650, I
506600 640, D, 680, I

```

```

* DRAIN STREAM
506500 700, U, 640, D

```

```

*          TEMP    PRESS    FLOW
*706100 33, 795.9 218.0 1.0E07 *HEATER DESING SPEC SHEET
*706100 33, 822.0 207.0 1.0E07 *PFL4 ACC TEST DATA
706100 33, 656.0 368.0 1.0E07 * PCU 5 HEAT BALANCE
706200 60 0.0 44400.0
706300 32
706500 30
706800 30

```

```

*          TEMP    PRESS    FEEDWATER FLOW
*706600 31 333.0 2260.0 1010750. * DESIGN SPEC DATA
*706600 31 340.0 2260.0 997000.0 * PFL 4 ACC TEST DATA
706600 31 357.0 1815.0 625000. * PCU 5 HEAT BALANCE

```

```

*          DRAIN INLET FLOW
*707000 31 408.1 437. 79920.0 *DESIGN SPEC SHEET
*707000 31 402.0 437. 74190.0 * PFL 4 ACC TESTET
707000 31 402.0 437. 0.0 * PCU 5 HEAT BALANCE

```

DESIGN MODE HEATER DATA

```

*          1          !2!          3          4          5
*          CTYPE    IDRAIN    IDXTGE    NMODFW    FRFWUT
706400 18 1 -620 4 0.0

```

```

*          6          7          8          9          10
*          IGFLC    IFFLC    IFLDFC    IFLGCR    HTRORT
*706400 2 2 0 0 1

```

```

*          11         12         13         14
*          IGFLDS    IFFLDS    IGFLDC    IFFLDC
*706400 2 2 2 2

```

```

*          CONDENSING SECTION DATA          THERM
*          1          2          3          4          5          6
*          DIDC    DODC    XLC    XNC    !XKTC!    SLC
706401 .527 .625 720. 402. 45. .8125

```

```

*          7          8          19!          10
*          DNZFWI    DNZFWO    DNZI    DNZO
706402 10.0 10.0 11.66 6.0
*          U VALU    PITCH    LEVEL
706403 0.0 0.0 0.0 795. .8125 5.0

```

```

*          DESUPERHEATING SECTION
*          1          2          3
*          XLDS    ?SBFLDS?    XBFLDS
706404 87.0 200. 4.
*          BAFFLE #

```

```

706405 0.0 1.0 1.0 0.0 0.0 113. * U VALUE

```

```

*          DRAIN COOLER SECTION
*          1          2          3
*          XLDC    ?SBFLDC?    XBFLDC
706406 72.0 200. 7.
*          BAFFLE #

```

```

706407 0.0 1.0 1.0 0.0 0.0 489. * U VALUE

```

END OF DECK

= 80 MW WESTINGHOUSE UNIT

```
*****
* DATA TAKEN FROM WESTINGHOUSE HEAT BAL. TEST #5, 4/18/55 *
* CUTLER PLANT UNIT # 5 *
* *
* CREATED: 02/08/91 REV. 0 BY: CNA *
* *
* REV #: 1 DATE: BY: *
* *
* DESCRIPTION: *
*****
```

```
*
*010200 NTGCRY NCEPRO NHOKUP NTURB NRHEAT NDEBUG BKALXR PPBEND
010200 2 3 1 2 0 0 0.0 -2.5
*
```

```
*
* ITRSPC ITRSCH ITRCON ITROPS ITRSTR ITREUP
012001 5 2 5 2 5 1 * ITERATION
* UPDATE CARD
*
```

```
*011010 IGENUM NGNTYP NGENER NGNCOL ISPEED BKGRAT POWFAC PPGNHZ PPGNHR
011010 1 2 2 0 3600 81176. 0.850 19.6 15.0
*
```

```
*011021 BKMCLI BKELEI
011011 0.0 0.0
*
```

```
*
* # OF ITERATIONS
* 012000 35
*
```

```
010001 1
```

```
*****
```

```
**** TABLE SUPPRESSION ****
```

```
*****
```

```
* SUPPRESS ALL 132-COLUMN TABLES
```

```
020000 NOPRINT
```

```
* 80 COLUMN TABLE SUPPRESSION CONTROL
```

```
020101 NOPRINT
```

```
020103 PRINT
```

```
020105 NOPRINT
```

```
020106 PRINT
```

```
020107 PRINT
```

```
020120 PRINT
```

```
020128 NOPRINT
```

```
020135 NOPRINT
```

```
020136 NOPRINT
```

```
020139 NOPRINT
```

```
020142 PRINT
```

```
020146 NOPRINT
```

```
020147 NOPRINT
```

```
020149 NOPRINT
```

```
020150 NOPRINT
```

```
020174 PRINT
```

```
*****
```





```

502700 250, T, 650, IA
502800 650, U, 330, I
502900 330, U, 260, T
503000 260, T, 270, T
503100 270, T, 510, I
504250 430, U, 210, T
504260 210, T, 440, I
* HTR INLET SOURCE
507000 700, U, 270, D

```

```

* HTR SOURCE
707000 31 402. 437. 0.0

```

\*\*\*\*\* SPECIAL STREAM \*\*\*\*\*

```

*
* STYPE PFAC1 * EXTRACTION LINE PRESSURE DROP
601450 2 0.173 * FWH #5 EXTRAC. PRESS. DROP

```

```

*
* TURBINE GROUPS: GS,HP,IP,LP
* USED GENERIC TYPE TURBINE (CTYPE=8)

```

GOVERNING STAGE

```

*
* CTYP NGEN NIPEN GEXT TYP MOIS NREND CASE DELPX
701000 8 1 0 0 1 0 1 5 0.0

```

```

*
* CTYP NGEN NXPEN GEXT TYPE MOIS NREND CASE DELXP
*
701100 8 1 0 1 2 0 1 5 0.0 #HP
701200 8 1 1 1 2 0 1 5 0.02 #HP
701300 8 1 3 1 2 0 1 5 0.02 #HP
701400 8 1 0 1 4 0 2 5 0.02 #LP
701500 8 1 1 1 4 0 2 5 0.02 #LP
*
701600 8 1 3 0 4 0 2 5 0.0 0.0 HEXT ANAREA 26.2

```

DESIGN DATA

```

*
* SHELL P SHELL H
701005 1017.0 1467.8 #1ST STG
701105 368.0 1340.6 #HP
701205 179.0 1271.0 #HP
701305 70.0 1199.4 #HP
701405 29.0 1145.5 #LP
701505 8.2 1076.0 #LP
701605 0.900 996.0 #LP

```

```

*
* PBIV HBIV MBIPV
701009 1271.0 1467.8 625000.
701109 1017.0 1467.8 615900.

```

701409 70.00 1199.4 509500.

\*  
\* END TURBINE GROUP

\* FEEDWATER HEATERS-----HEAT EXCHANGERS-----CONDENSER

	FEEDWATER HEATERS							
	CTYPE	IDRAIN	IDXTGE	NMODFW	FRFWUT	TTD	DCA	*HTR #
702300	16	1	150	2	0.0	6.5	10.5	* 1
702400	16	0	140	2	0.0	14.5	9.5	* 2
702500	17	1	130	2	0.0	10.5		* 3
702600	18	1	120	2	0.0	16.0	11.5	* 4

\* DESIGN MODE HEATER DATA

	1	12!	3	4	5
	CTYPE	IDRAIN	IDXTGE	NMODFW	FRFWUT
702700	18	1	-110	4	0.0

	6	7	8	9	10
	IGFLC	IFFLC	IFLDFC	IFLCCR	HTRORT
*702700	2	2	0	0	1

	11	12	13	14
	IGFLDS	IFFLDS	IGFLDC	IFFLDC
*702700	2	2	2	2

	CONDENSING SECTION DATA					THERM COND.
	1	2	3	4	5	6
	DIDC	DOOC	XLC	XNC	!XKTC!	SLC
702701	.527	.625	600.	402.	14.5	.8125

	7	8	19!	10		
	DNZFWI	DNZFMD	DNZI	DNZO	U VALU	PITCH
						LEVEL
702702	10.0	10.0	11.66	6.0		
702703	0.0	0.0	0.0	795.	.8125	5.0

\* DESUPERHEATING SECTION

	1	2	3
	XLDS	?SBFLDS?	XBFLDS
702704	87.0	200.	4.
			BAFFLE #

\* 702705 0.0 1.0 1.0 0.0 0.0 113. \* U VALUE

\* DRAIN COOLER SECTION

	1	2	3
	XLDC	?SBFLDC?	XBFLDC
702706	72.0	200.	7.
			BAFFLE #

\* 702707 0.0 1.0 1.0 0.0 0.0 489. \* U VALUE

```

*
*           HEAT EXCHANGERS
*      CTYPE  TTHXDN  FRHXUT
*
702200  20    0.0    0.0    * SJAЕ
*
*           CONDENSER
*      CTYPE  IDRAIN  NMODFW  FRFWUT  PPSH
*
702100  10    1      2      0.0    0.890
*
*
*      END FEEDWATER HEATERS---HEATEXCHANGERS---CONDENSER
*
*
*           PUMPS:   COND.---HDP---BFP
*
*      CTYPE  PMPDIS
703100  41    308.0  * COND.
703200  41    280.0  * HDP
703300  41    1820.0 * BFP
*
*      END PUMPS
*
*
*           VALVES
*      CTYPE  PDRPL  PDRFP  PDRPV  TFRIST  PTHV  HTHV  WTHV
*
704100  35    -2.0  -2.0  -2.0  0.30  1271.0  1467.8  624100.
*
*      CTYPE  PDVS
*
*
*      END VALVES
*
*
*           SOURCES / SINKS
*
*      CTYPE  TTVSC  PPSVC  MWVSC  THERM
*
704400  30
704300  31    70.0  20.0  1.30E7  0.0  * CIRC H2O FLOW
705100  32
*
705000  33    950.0  1271.0  625000.  * HS FLOW
*
*      *****
*
*      END SOURCES / SINKS
*
*
*           MIXER DISCRIPTION
*
*      CTYPE  IFLPRU  PPMIXU
*
706400  50    1
706600  50    1

```

```

706700      50      1
706500      50      1
*
*           END MIXER DISCRIPTION
*
*           SPLITTER DESCRIPTION
*
*           CTYPE      HMFIXB      WMFIXB
706100      61         0.0         900.0
*
*           -MIN DATA
*           CTYPE      PACLEK      WMFIXB      PPREC
706200      64         5111.1      8100.0      1017.0 * LO TO 17TH STG HTR
706300      64         631.1       1000.0      1017.0 * LO TO 28TH STG HTR
*
*           END SPLITTER DESCRIPTION
*
*           CALC. OF LO CONSTANT   * C *
*
*           CXVAR      NXUIDC      VALYC      YCNVRG      CYFLTR      CYVAR      NYUIDC
*
840100      PACLEK, 620,      8100.0,  1.0E-3,  1.0,      MN,  153
840200      PACLEK, 630,      1000.0,  1.0E-3,  1.0,      MN,  152
*           END OF INPUT DATA
*
*
*

```