

Utilization of the Hawthorn 5 PEPSE[®] Boiler Model

David P. Williams

Kansas City Power & Light Company

Abstract

Kansas City Power & Light Company determined the need to acquire a static modelling program to predict the performance of their steam generating units. The PEPSE modelling program was chosen for this purpose.

Since its development, the PEPSE predictive boiler model at Hawthorn Unit 5 has been used to develop a new predictive performance data sheet and to analyze the thermal effects of burning various coal types in the unit. Hawthorn presently performs actual "test burns" of coal types to see how operating parameters are affected by burning these coals. Data was gathered during a recent test burn to validate the predicted performance from the PEPSE boiler model. In the future, it is hoped that PEPSE can be utilized to eliminate actual test burns on the unit and to aid in the selection of the best fuel for Hawthorn Unit 5.

Introduction

Kansas City Power & Light Company purchased an on-line performance modelling program in 1985. This modelling program is called PMAX and is used to monitor boiler, turbine, and feedwater heater performance while a unit is on-line. As of this date, PMAX is being utilized at each of our coal-fired units.

In July '90 discussion began concerning the need to model and predict changes in operating parameters before they actually occurred. We wanted a way to study the effect of verifying operating conditions on the unit and to assess the impact of equipment changes on plant efficiency. PEPSE was chosen as the modelling tool to accomplish this. Initially, the PEPSE turbine model was developed for each plant. These are very useful but it was felt that a boiler model for each of KCPL's units would provide a much more useful and predictive tool. In May of 1991, a PEPSE boiler model class was given to the Performance Engineers at each station. Each engineer was charged with developing a working model of their respective boilers.

The boiler at Hawthorn was originally designed to burn a high Btu (11,000 Btu/lb.) Illinois bituminous coal. This type of coal was never burned at this station. Presently, Hawthorn is burning several Powder River Basin coals on the unit. Heating values are in the range of 8500 - 8800 Btu's/lb. with a very low sulfur content of 0.5% or less. The original equipment manufacturer provided a "Predicted Performance Sheet" based on the use of the Illinois coal. This sheet contained many of the operating temperatures and pressures that the unit could be expected to produce while burning the Illinois coal. Since Hawthorn has never burned this type of fuel, this performance sheet was rather useless. Comparisons to actual data were virtually impossible. Thus, the need was recognized to utilize the Pepse boiler model to develop a new "Predicted Performance Sheet" for the unit based on the burning of

western fuels. This would allow some comparisons to be made with the expected and actual performance parameters.

In addition to developing a new predictive performance sheet for the unit, the PEPSE boiler model was asked to predict the performance of burning various fuel types in Hawthorn Unit 5. Hawthorn has had the opportunity in the past to take advantage of low cost spot fuel purchases. These purchases have usually resulted in poor performance of the unit or increased shutdowns of the unit due to various reasons. Hawthorn Station wanted a predictive modelling tool(s) to aid in the selection of the fuel types before purchasing them. Currently, Hawthorn conducts "test burns" of the fuel types in the boiler, usually with poor results. It is hoped that the PEPSE boiler model (along with other models being developed, i.e., CQIM, etc.) can eliminate the need to run test burns of coals and predict which coals may best be utilized in the unit.

KCPL & Hawthorn Station Background

KCPL's capacity is about 70% coal-fired and 14% natural gas burning combustion turbines used for peaking. The remaining is nuclear capacity from the Wolf Creek Plant which began operation in 1985. Hawthorn operates as part of KCPL's five-plant 3,028 MW generating system. These power facilities produce electricity for over 400,000 customers in KCPL's 4,700 square mile service territory. Hawthorn represents almost 15% of the Company's total production capacity. Hawthorn Units 1-4 were completed between 1951 and 1955 and are on permanent shutdown. The last Hawthorn addition - Unit 5 in 1969 - was KCPL's first large-scale, modern generating unit, providing significant economies of scale. Its current rated capacity is 477 megawatts but has a generator rating of 514 megawatts.

The steam generator is a Combustion Engineering forced flow,

tangentially fired unit. (Fig. 1) There are six type 803 RPS pulverizers on the unit with a mill flow rate of 42 tons/hour each. The design steam capacity at the maximum continuous rating load is 3,500,000 lb/hr. The tubing geometry in the boiler includes radiant and convective superheat and reheat assemblies. A continuous finned, staggered economizer (a source for pluggage to occur) was also designed into the unit. The unit was also originally designed and operated as a forced draft unit. The change to a balance draft unit occurred in 1978.

Boiler Model Construction

The construction of the boiler model for Hawthorn Unit 5 began with the developed boiler model example in the PEPSE boiler modelling class. This model was developed by Gene L. Minner of Halliburton/NUS. The model geometries of the boiler example in the class and that of Hawthorn Unit 5 are exactly the same. This simplified much of the boiler modelling. Many of the same assumptions were used as in the class example. Information required to construct the boiler model came from several sources including plant drawings, design information, contract data and construction memos. A simplified boiler model was first constructed to test the boundary conditions. (Fig. 2) Once this model converged and the output matched the vendor's predicted temperatures and pressures, the detailed boiler model was then constructed. The detailed boiler model incorporated all the separate components for each of the major boiler sections. (Fig. 3) The tube geometry and passage dimensions were identified and entered into the component sections. The detailed boiler model was then run and the output checked against the design load data. Fine tuning of the Hawthorn 5 model was difficult due to the lack of data for the various boiler stages. It appears that the original equipment manufacturer was becoming aware that other organizations could develop a computerized performance

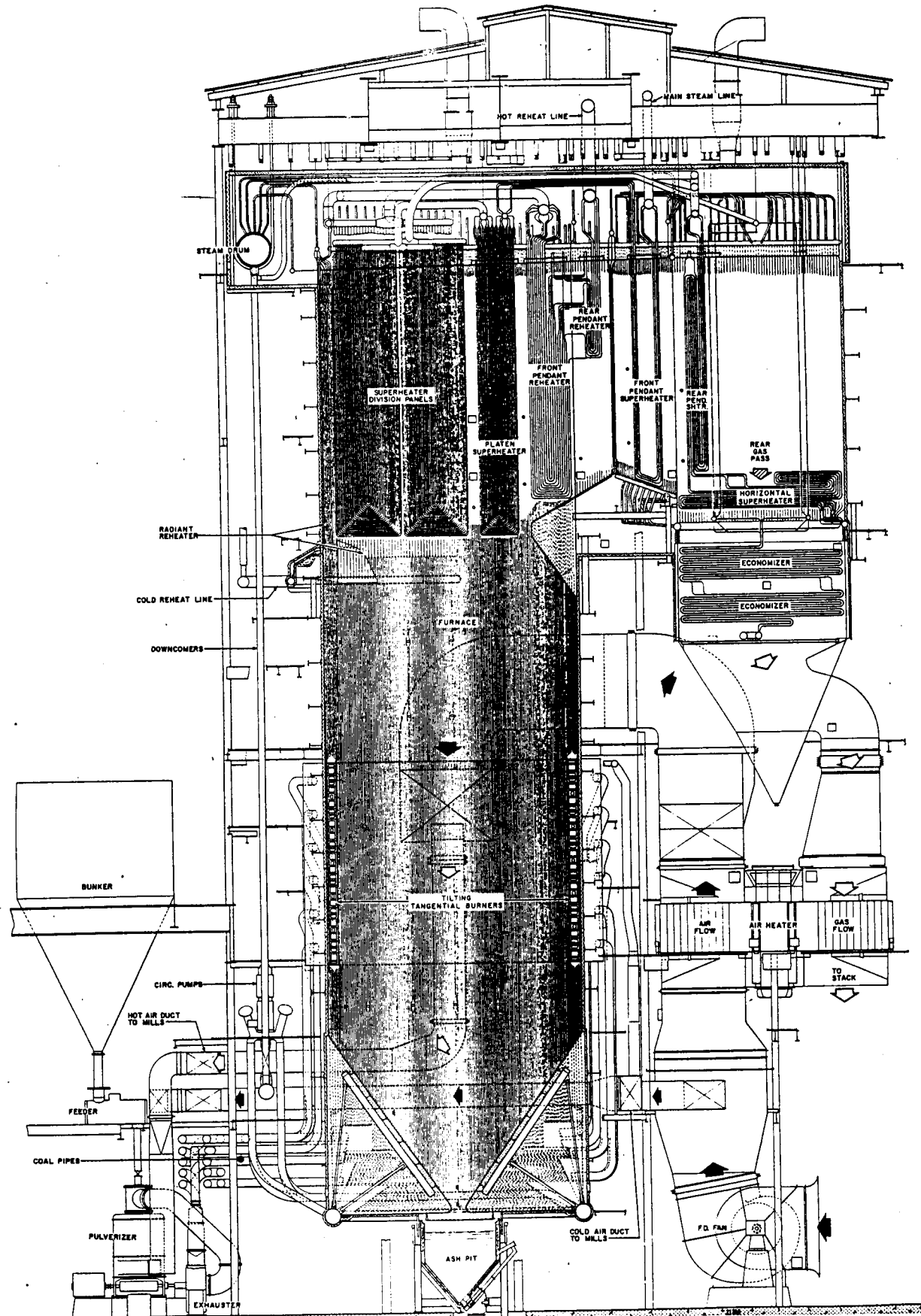
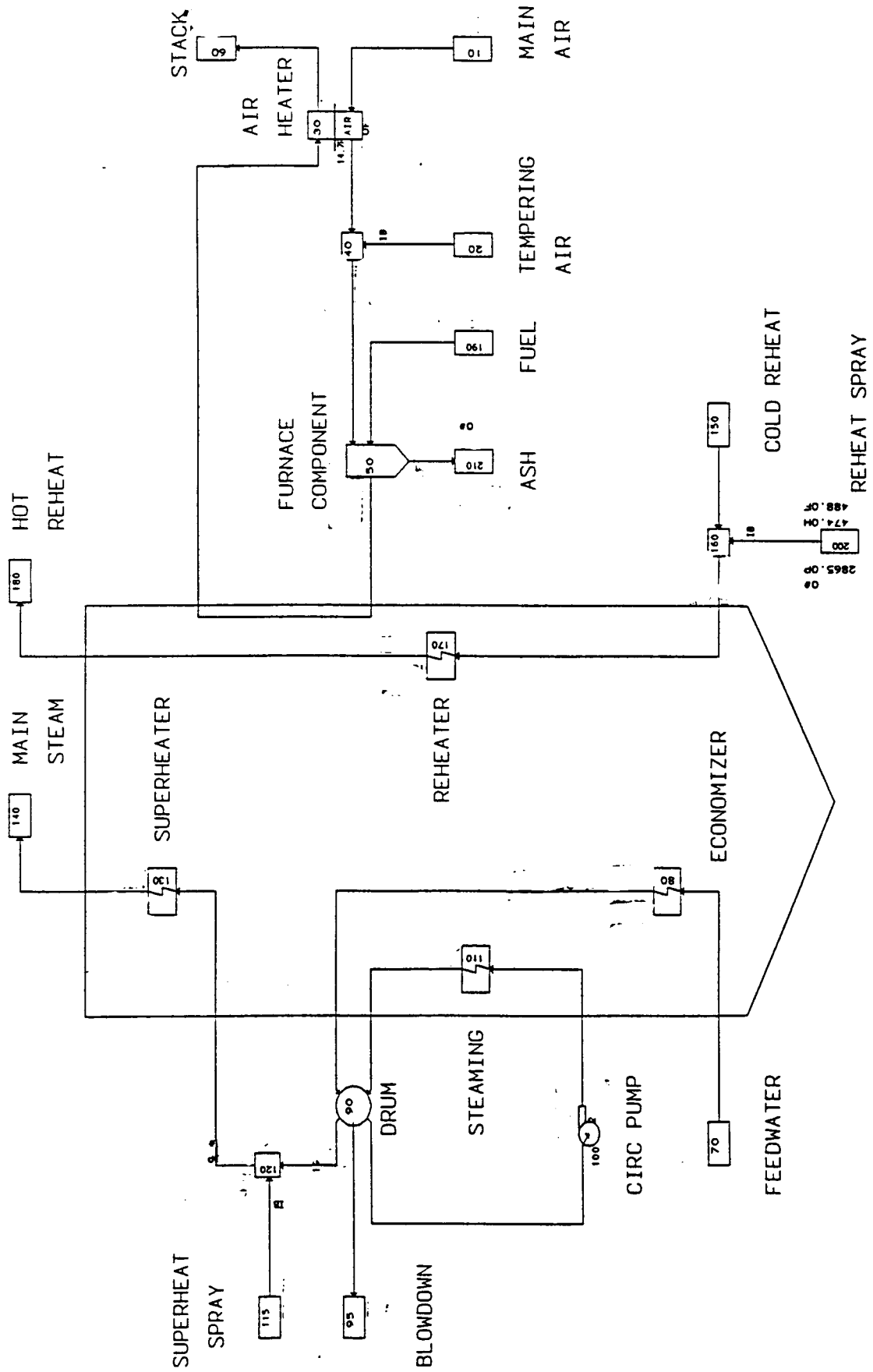


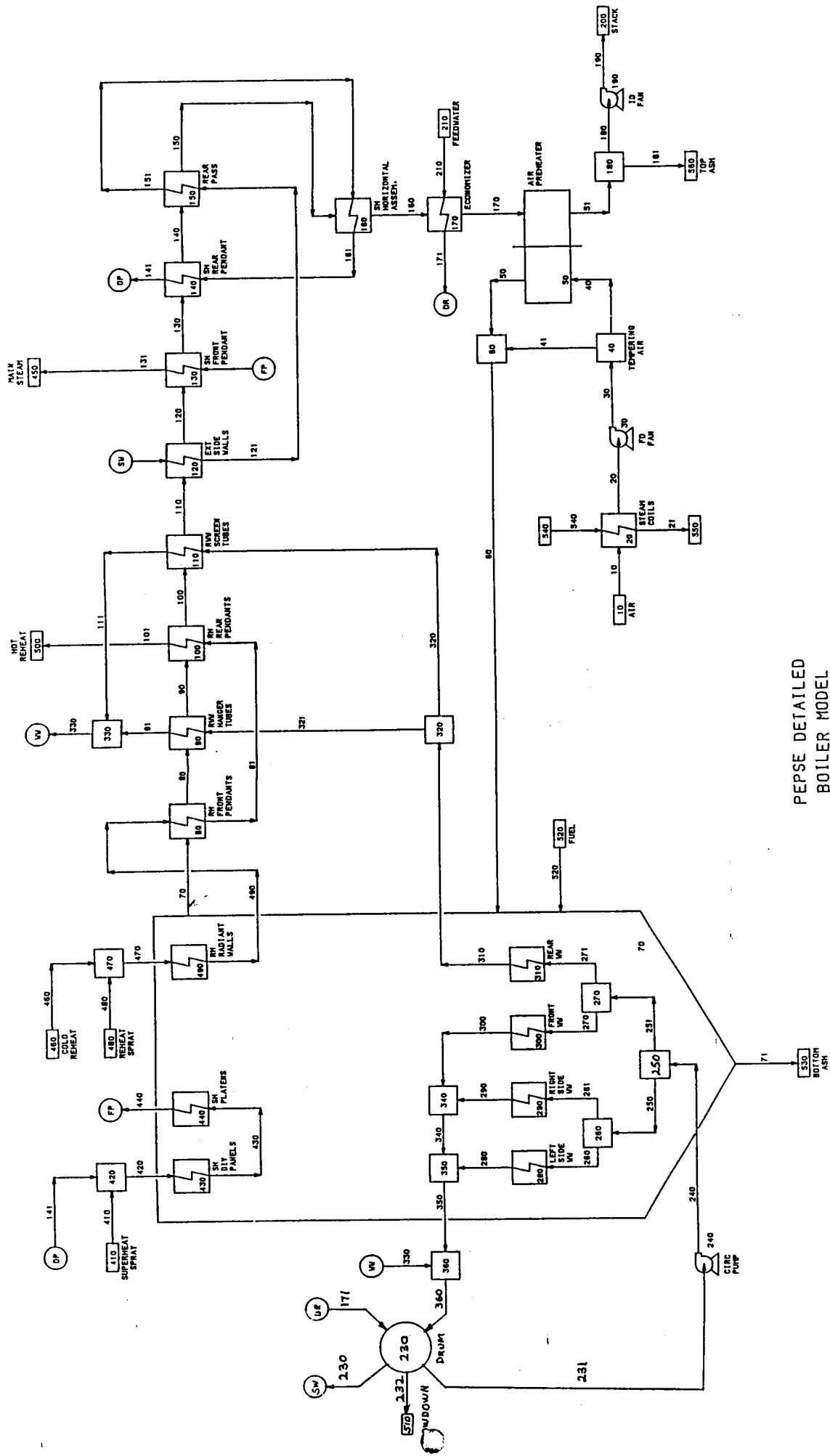
Fig. 1

Hawthorn Unit 5
 Combustion Engineering, Inc.



PEPSE SIMPLIFIED BOILER MODEL

Fig. 2
Hawthorn Unit 5, 9/91



PEPEE DETAILED
BOILER MODEL

Fig. 3
Hawthorn Unit 5, 10/91

model. They reduced dramatically the amount of information on their predicted performance sheet. Our Montrose units, built in the late 50's, contain much more thermal data on their data sheets, making fine tuning much easier. HTC multipliers, fouling factors and form loss coefficients were determined where information was available. If operating parameters were available^{UN}, preliminary values given in the boiler model training handbook were used. Once the detailed boiler model converged, a check against the vendor's predicted performance values validated the model. The fine tuned detailed boiler model was developed for operating conditions at the maximum continuous rating (MCR) and the control load point.

For comparing the desired values with the actual values and adjusting the levels of fuel, air, and water to match the desired values, a "control system" had to be incorporated into the model. Four PEPSE controls were used to simulate the boiler "control system"¹:

Desired Value	Controlled Value
Steam Pressure	Drum Pressure
Steam Temperature	Attemperation Flow
Drum Exit Quality	Feedwater Flow
Hot Reheat Temperature	Furnace Exit Temperature

With the control system in place, the boiler model was completed and ready to do some preliminary analyses. The complete boiler model input is included as an appendix to the paper.

Boiler Model Utilization

A. New Predicted Performance Data Sheet

Hawthorn Unit 5 was built in 1969. The design of the unit was

¹PEPSE Boiler Modelling Seminar Notebook, Halliburton/NUS.

developed by Combustion Engineering. With the development of the boiler design, C.E. provided in the boiler instruction manual, a data sheet that indicated the predicted performance of the boiler. (Fig. 4) Since 1969, this was the only gauge operating personnel used to judge the performance of the boiler and the values used were based on a coal type that was never used in the boiler. The high cost of this Illinois bituminous coal made it uneconomical to burn at Hawthorn. Coal from Oklahoma was burned from 1969 - 1985.

Hawthorn switched to burning a western Powder River Basin coal in 1986. This was in response to environmental concerns and the favorable fuel prices of western fuels. With this new type of fuel being burned in the unit, a new data sheet needed to be developed.

After matching Combustion Engineering's predicted performance values at the control load and MCR for the design coal, the representative western coal (Black Thunder) ultimate analysis was entered as the fuel source (component 520) and the evaporation flow, temperature, and pressure utilized as the independent variable or output desired. An estimate was made on the quantity of air flow entered into the boiler. The results of the PEPSE runs can be seen in Fig. 5. The most interesting result was seen in the amount of fuel that is required to meet the steam demand. At a rated steam flow of 3,500,000 lb/hr., the western fuel required was 134,145 lb/hr. more than the original design fuel. The required mill flow rate was 3 tons/hr. higher than what the mills were designed to deliver. Boiler efficiency also decreased by 2-3% at the two load points. After looking at these results, it was decided to try and let PEPSE tell us how much steam flow (or megawatt load) the unit could generate with the western fuels. The results indicated the unit could supply 3,124,803 lb/hr of steam. This is 89.2% of the rated design steam flow. The rated megawatt loading at full steam flow is 515 megawatts. The new predicted steam flow coordinates to a loading of 460 megawatts. The unit is presently rated at 477

KANSAS CITY POWER & LIGHT COMPANY
HAWTHORNE STEAM ELECTRIC STATION
UNIT NO. 5

ORIGINAL C-E CONTRACT NO. 21765 – CCRRP
POWER SYSTEM SERVICES CONTRACT 59776

PREDICTED PERFORMANCE*

		Control Load	Max. Cont. Load	Max. Cont. Load
Fuel		COAL		GAS
Evaporation	lb/hr	1,667,000	3,500,000	3,500,000
Feedwater Temperature	F	413	483	483
Superheater Outlet Temperature	F	1,005	1,005	1,005
Superheater Outlet Pressure	psig	2,500	2,625	2,625
Superheater Pressure Drop	psi	55	200	200
Reheater Flow	lb/hr	1,507,000	3,120,000	3,120,000
Reheater Inlet Temperature	F	536	627	627
Reheater Inlet Pressure	psig	275	581	581
Reheater Outlet Temperature	F	1,005	1,005	1,005
Reheater Pressure Drop	psi	16	31	31
Economizer Pressure Drop	psi	4	20	20
Air Drop Cold Air Duct to A.H. Outlet	"wg	1.10	4.10	3.5
Air Drop Hot Air Duct to Windbox	"wg	0.35	1.30	1.10
Air Drop through Windbox **	"wg	2.0-5.0	3.5-5.0	3.5-5.0
Furnace Pressure	"wg	-0.10	-0.10	-0.10
Gas Drop, Furnace to Econ. Outlet	"wg	2.00	7.65	6.05
Gas Drop, Econ. Outlet to A.H. Outlet	"wg	1.80	5.60	5.00
Gas Temp. Entering Air Heater	F	565	670	665
Gas Temp. Leaving Air Heater, Uncorr.	F	236	268	251
Gas Temp. Leaving Air Heater, Corr.	F	246	258	241
Air Temp. Leaving Air Heater	F	125	102	90
Air Temp. Leaving Air Heater	F	527	601	599
Ambient Air Temperature	F	80	80	80
Excess Air Leaving Economizer	%	20	20	10
Fuel Fired	lb/hr CFH	211,900	409,700	4,960,000
Efficiency	%	90.07	89.08	85.44

***NOTE:** These performance figures are predicted only and are not to be construed as being guaranteed except where the points coincide with the guarantees.

Superheat steam temperature control range is from 1,667,000 to 3,500,000 lb/hr.

Reheat steam temperature control range is from 1,507,000 to 3,120,000 lb/hr.

**Adjustable for favorable firing conditions.

The fuel specifications on which the guarantees are based are as follows:

Mid-West Bit.	HHV = 11,315 BTU/LB
F.C.	44.35%
Vol.	34.92
Ash	8.86
Moist.	11.87
Total	100.00%

Fig. 4

**KANSAS CITY POWER & LIGHT COMPANY
HAWTHORN UNIT NO. 5 STEAM ELECTRIC STATION
ORIGINAL C.E. CONTRACT NO. 21765**

PREDICTED PERFORMANCE* FUEL	CONTROL LOAD		MAX. CONT. LOAD		LOAD WITH MILL DESIGN FLOW RATE
	DESIGN COAL	WESTERN COAL	DESIGN COAL	WESTERN COAL	WESTERN COAL
Evaporation lb/hr	1,667,000	1,667,000	3,500,000	3,500,000	3,124,803
Feedwater Inlet Temp. °F	413	413	483	483	483
Feedwater Outlet Temp. °F	544	547	607	613	619
Economizer Press. Drop psi	4	4	20	20	16.5
Furnace Exit Temp. °F	2,207	2,174	2,416	2,375	2,483
Superheater Outlet Temp. °F	1,005	1,005	1,005	1,005	1,005
Superheater Outlet Press. psig	2,500	2,500	2,625	2,625	2,604
Superheater Spray Flow lb/hr	89,944	91,982	84,615	108,213	179,401
Superheat Temp. Aftr Spray Flow °F	765	766	792	795	795
Reheater Flow lb/hr	1,507,000	1,507,000	3,120,000	3,120,000	2,888,096
Reheater Inlet Temp. °F	536	536	627	627	572
Reheater Inlet Press. psig	275	275	581	581	555.4
Reheater Outlet Temp. °F	1,005	1,005	1,005	1,005	1,005
Reheater Pressure Drop	16	16	31	31	23
Air Flow lb/hr	2,768,183	2,740,506	4,694,500	4,745,203	4,412,524
Gas Flow lb/hr	2,379,835	2,420,298	4,603,955	4,788,802	4,413,523
Gas Temp. Enter. A.H. °F	564	567	668	675	669
Gas Temp. Exit. A.H. (Corr.) °F	240	252	258	274	271
Gas Temp. Exit. A.H. (Uncor.) °F	268	281	275	290	289
Air Temp. Enter. A.H. °F	125	125	102	102	102
Air Temp. Exit. A.H. °F	538	546	604	617	614
Ambient Air Temp. °F	80	80	80	80	80
Excess Air Leaving Econ. %	20	20	20	20	20
Fuel Fired lb/hr	211,652	279,792	409,455	543,600	501,000
Mill Flow Rate Tons/hr	17.64	23.32	34.12	45.30**	41.75
Boiler Efficiency %	89.50	87.10	88.90	86.05	86.11
The fuel specs. on which the predicted performance is based on are as follows:	Mid-West Bit.	Black Thunder	*The predicted performance values were generated by PEPSE Performance Modelling System. **Beyond Mill Design Flow Rate		
HHV Btu/lb	11315	8800			
Moisture %	11.87	28.00			
Ash %	8.86	4.90			
Sulfur %	3.38	0.34			
Fixed Carbon %	44.35	35.40			

Fig. 5

megawatts but recently have only been able to load up to around 455 megawatts. This gives credence to PEPSE's output. The new predicted performance sheet will be placed in the Boiler Instruction Manuals. After the Spring 1992 overhaul, Hawthorn is planning to run tests to compare the PEPSE results with the actual performance parameters. Thermowells are being installed in the inlet and outlet headers of the boiler sections. This information will help define the tuning factors that are required to more accurately model the system. Once completed, this new Predictive Performance Data Sheet will be the basis for comparison of the Hawthorn Unit 5 performance.

B. Fuel Type Predicted Performance

The Hawthorn 5 PEPSE boiler model was asked to predict the performance of the boiler with various fuel types. Hawthorn was preparing to perform some actual "test burns" of several coal types. These tests required the burning of approximately 30,000 - 60,000 tons of each coal type. Without knowing how the boiler would react to the fuel, the station was at risk of having deratings of the unit or increased forced outages if the fuel was incapable of burning. In addition to the potential for increased operating and maintenance expenses, there was a substantial amount of data that must be gathered by the various departments at the station (i.e., Fuel, Operations, Results, and Engineering departments). The need for a boiler model that could predict the performance was needed at Hawthorn Station.

Two PEPSE runs were made of the three coal types Hawthorn was planning to burn at the station. The first run was to predict the fuel usage and boiler efficiency at the maximum continuous rating (MCR). This, for Unit 5, was a steam flow of 3,500,000 lb/hr. The other PEPSE run was made with the same fuel flow at the time the Central Testing Crew was performing boiler efficiency tests on the test fuels. The results from this run would tell us the maximum

steam flow and boiler efficiency for the same amount of fuel during the performance tests. The run results could then be compared with the test results to see how well the boiler model matched the actual test results.

Following is a table of the PEPSE projected results and the results taken by KCPL's Central Testing Group:

	Coal Type A			Coal Type B			Coal Type C		
	PEPSE @ MCR	Actual Results	PEPSE w/ Same Fuel Amount	PEPSE @ MCR	Actual Results	PEPSE w/ Same Fuel Amount	PEPSE @ MCR	Actual Results	PEPSE w/ Same Fuel Amount
Firing Rate (lb/hr)	569023	527200	527200	569662	521800	521800	532953	532000	532000
Boiler Efficiency (%)	85.6	84.10	85.9	85.4	83.1	85.1	86.5	84.0	86.1
Exit Gas Temperature (°F)	678	761	665	680	770	663	669	761	666
Superheat Spray Flow (lb/hr)	122566	186270	90530	126521	272560	101719	93591	165120	63227
Main Steam Flow (Klb/hr)	3,500	2,975	3,375	3,500	2,998	3,211	3,500	2,980	3,519

The results from both the PEPSE runs and the tested parameters show some discrepancies and similarities.

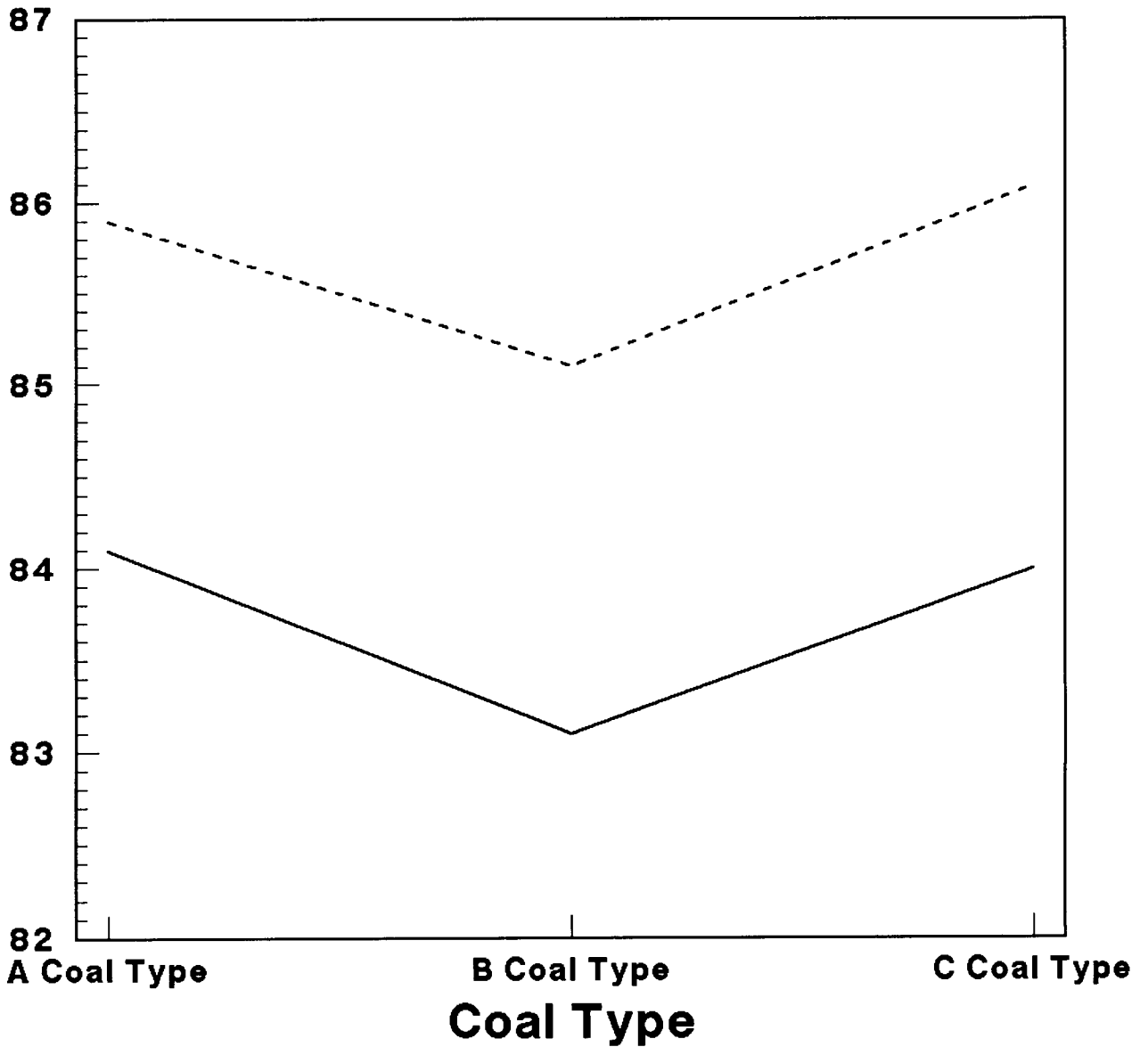
Boiler efficiency, although the tested amounts were lower, still showed the same trend as what was predicted by PEPSE. (See Fig. 6).

The other parameters that could be compared, including boiler efficiency, all differ from the PEPSE results. This may be due to several reasons:

1. The boiler at the time of the tests was beginning to plug severely in the backpass of the boiler. This will cause exit gas temperatures to rise, O₂ levels to rise and heat transfer to decrease thereby reducing the tested boiler efficiency.
2. The tested results are averaged over a 2 hour period. During this time frame,

**Comparison Of
Tested and PEPSE Generated
Boiler Efficiency**

Efficiency %



Tested Results **PEPSE Results**
——— - - - - -

Fig. 6
2-13

boiler upsets may occur thus affecting the final results.

3. The heat transfer coefficient multipliers originally developed could be incorrect and more data input is required to correctly predict these multipliers.
4. The two lowest pressure feedwater heaters were out of service at the time of the test. This causes the boiler to utilize more fuel to raise the feedwater temperature thereby reducing boiler efficiency.

In conclusion, it appears that several areas need to be addressed before the developed PEPSE boiler model can be used to make final economic decisions on the coal type to burn at Hawthorn Unit 5. Testing procedures and boiler conditions must be standardized for comparison; the heat transfer coefficient multipliers must be further fine tuned in the model to more accurately model the heat transfer occurring in the various sections; and operating parameters (O_2 , air heater exit gas temperature, etc.) that are more indicative of actual conditions occurring in the boiler must be utilized in the model.

It should be stated that the present model does indicate trends that occur between various coal types and thus the initial objectives in developing the model have been met. These initial trial runs of the PEPSE boiler model will serve as a basis for further refinement.

Future Uses of the Boiler Model

The advantages of having a working boiler model are clearly defined for Hawthorn and KCPL. Specifically at Hawthorn, there are several areas in which the PEPSE boiler model will be utilized in

the near future.

1. Presently, the economizer on Unit 5 is of the continuous finned, staggered tube design. This design is very susceptible to pluggage. There are several tubing geometry alternatives available; some requiring more heat transfer surface. PEPSE will be asked to determine what the change in tubing geometry will do to boiler operation, construction requirements (more tubes needed) and boiler efficiency.
2. The boiler on Unit 5 has a tendency to foul in certain sections of the boiler. Heat transfer coefficient multipliers may be manipulated to simulate the fouling in these areas and determine how and to what degree this affects the performance of the unit. This can help Hawthorn concentrate their maintenance and construction efforts in areas that have the most impact.
3. Operating parameters such as excess air, spray flows and combustion air conditions will be manipulated in the boiler model to investigate the effects on overall performance.
4. The Central Testing Group at KCPL has interest in using the PEPSE boiler model to assess their testing results. Presently, no comparison except to past data can be made.
5. Several plant operating problems (low reheat temperatures, high exit gas

temperatures, etc.) need to be analyzed and corrected. Before initiating actual changes in the boiler, PEPSE can show the effects on the boiler performance and aid in the decision making process.

Summary

Kansas City Power & Light Company recognized the need to develop working predicted performance boiler models at their generating stations. A preliminary model was developed for Hawthorn Unit 5. This model has been used to develop a new predicted performance data sheet for the unit based on the current coal type the unit is burning. The past data sheet was for a design coal that never was burned at the station. The new predicted data sheet will be fine tuned as data instruments are installed in the boiler.

The second use of the model has been to compare the predicted performance of several coal types for making economical fuel choices. Although further refinement is needed, the model does produce preliminary results that can aid in the selection of fuel types prior to performing costly test burns.

In the future, the PEPSE Boiler Model will be fine tuned to perform tube geometry predictions, assess test data, and to eliminate operating problems.

REFERENCES

1. PEPSE Boiler Modelling Seminar Notebook, Halliburton/NUS Energy Group, P. O. Box 50736, Idaho Falls, Idaho, 5/1/91.
2. Hawthorn Steam Electric Station Unit 5 Boiler Instruction Manual:, Vol. 1, Combustion Engineering, Inc., 1000 Prospect Hill Road, Windsor, Connecticut, 10/68.
3. Hawthorn Station Information Guide, Kansas City, Power & Light Company, P. O. Box 418679, Kansas City, MO 64141-9679.

010001 80 * 80 column output

*
* PEPSE USER : ADMIN
* DATE : 04/28/92
* TIME : 12:13
* MODEL FILE ID : H5MCR1
* JOB FILE ID : \EASEPLUS\DEMO\H5MCRT1.JOB
* RESULTS FILE ID : \EASEPLUS\DEMO\H5MCRT1.OUT
*

= (DPW) HAWTHORN UNIT 5 BOILER MODEL (NO FRILLS, DESIGN MODE COMPOS)

*
* THE TYPE 1 STREAMS ACCOUNT FOR ELEVATION, FRIC, FORM IN CIRC LOOP.
* SINGLE DOWNCOMER STREAM REPRESENTS 9 PARALLEL PIPES. CAN MATCH ONLY
* VELOCITY AND L/D, BUT NOT REYNOLDS NUMBER.
*

* GENERIC INPUT DATA

* CYCLE FLAGS

010200 0 0 0 0 0 0 0. 0.

* CYCLE CONVERGENCE DATA

012000 50 0. 0. 0. 0. 0. 10 500000.

* SPECIAL FEATURES INITIATION DATA

012001 5 2 10 0 0 0

* SPECIAL FEATURES CALCULATIONAL ORDER DATA

012002 0 0 0

* PEPSE OUTPUT SUPPRESSION CARDS

*
020000 PRINT
020002 NOPRNT
020004 NOPRNT
020005 NOPRNT
020014 NOPRNT
020015 NOPRNT
020016 NOPRNT
020021 NOPRNT
020022 NOPRNT
020023 NOPRNT
020025 NOPRNT
020028 NOPRNT
020029 NOPRNT
020034 NOPRNT
020037 NOPRNT
020038 NOPRNT
020042 NOPRNT
020050 NOPRNT
*

*** MODEL GEOMETRY

*
500100 10, U, 20, S
500200 20, D, 30, I
500210 20, T, 550, I
500300 30, U, 40, I
500400 40, U, 50, T

500410	40,	B,	60,	IB
500500	50,	T,	60,	IA
500510	50,	D,	180,	I
500600	60,	U,	70,	IA
500700	70,	U,	80,	S
500710	70,	B,	530,	I
500800	80,	D,	90,	S
500810	80,	T,	100,	T
500900	90,	D,	100,	S
500910	90,	T,	330,	IB
501000	100,	D,	110,	S
501010	100,	T,	500,	I
501100	110,	D,	120,	S
501110	110,	T,	330,	IA
501200	120,	D,	130,	S
501210	120,	T,	150,	T
501300	130,	D,	140,	S
501310	130,	T,	450,	I
501400	140,	D,	150,	S
501410	140,	T,	420,	IA
501500	150,	D,	160,	S
501510	150,	T,	160,	T
501600	160,	D,	170,	S
501610	160,	T,	140,	T
501700	170,	D,	50,	S
501710	170,	T,	230,	FW
501800	180,	U,	190,	I
501810	180,	B,	560,	I
501900	190,	U,	200,	I
502100	210,	U,	170,	T
502400	240,	U,	250,	I
502500	250,	U,	260,	I
502510	250,	B,	270,	I
502600	260,	U,	280,	T
502610	260,	B,	290,	T
502700	270,	U,	300,	T
502710	270,	B,	310,	T
502800	280,	T,	350,	IB
502900	290,	T,	340,	IB
503000	300,	T,	340,	IA
503100	310,	T,	320,	I
503200	320,	U,	110,	T
503210	320,	B,	90,	T
503300	330,	U,	360,	IB
503400	340,	U,	350,	IA
503500	350,	U,	360,	IA
503600	360,	U,	230,	RI
502300	230,	ST,	120,	T
502310	230,	DC,	240,	I
502320	230,	BD,	510,	I
504100	410,	U,	420,	IB
504200	420,	U,	430,	T
504300	430,	T,	440,	T
504400	440,	T,	130,	T
504600	460,	U,	470,	IA
504700	470,	U,	490,	T
504800	480,	U,	470,	IB
504900	490,	T,	80,	T
505200	520,	U,	70,	IF
505300	540,	U,	20,	T

*
*

* COMPONENT DATA

*
***** HEAT EXCHANGERS
*

* STEAM COILS

700200 20 102.

700201 0. 0. 0. 0. 0. 0. 0.

* REHEATER FRONT PENDANT

700800 28 1 3120000. 595.700012 856.

700804 3 1 1 50. 52.25 42. 20.

700805 65. 2. 2.17 2.5 4.5 9.5 0.

700806 0. 0.9 20. 0. 9.22e-5 0.

700807 0. 0. 0. 0. 0. 0.

700808 0. 0. 0.0 0. 0. 0. 0.

* REAR WATERWALL HANGER TUBES

700900 28 1 2059000. 2859.699951 0.2

700904 3 0 3 42.700001 52.25 42.700001 1.

700905 61. 1. 1.57 2.25 2.25 9.5 0.

700906 0. 0.9 20. 0. 0.000127 0.

700907 0. 0. 0. 0. 0. 0.

700908 0. 0. 0.0 0. 0. 0. 0.

* REHEATER REAR PENDANT

701000 28 1 3120000. 595.700012 552.

701004 3 0 1 43. 52.25 18. 10.

701005 131. 2. 2.2 2.5 4.375 4.75 0.

701006 0. 0.9 20. 0. 9.091e-5 0.

701007 0. 0. 0. 0. 0. 564.700012

701008 0. 0. 0.0 0. 0. 0. 0.

* REAR WATERWALL SCREEN TUBES

701100 28 1 5040000. 2859.699951 0.2

701104 3 0 3 40. 52.25 40. 3.

701105 162. 1. 1.855 2.375 3.25 3.847 0.

701106 0. 0.9 20. 0. 0.000108 0.

701107 0. 0. 0. 0. 0. 0.

701108 0. 0. 0.0 0. 0. 0. 0.

* EXTENDED SIDE WALLS

701200 28 2 1219200. 2859.699951 1. 1.

701201 0. 0. 0. 0. 0. 0.

701202 0. 0. 0.0 0. 0.

* SUPERHEATER FRONT PENDANT

701300 28 1 3500000. 2859.699951 909.

701304 3 0 1 43. 52.25 42. 8.

701305 131. 2. 1.405 2.125 4. 4.75 0.

701306 0. 0.9 20. 0. 0.000142 0.

701307 0. 22532. 0. 0. 0. 0.

701308 0. 0. 0.0 0. 0. 0. 0.

* SUPERHEATER REAR PENDANT

701400 28 1 3500000. 2859.699951 909.

701404 3 0 2 43. 52.25 39. 12.

701405 156. 3. 1.4 2. 4. 4. 0.

701406 0. 0.9 20. 0. 0.000143 0.

701407 0. 49192. 0. 0. 0. 0.

701408 0. 0. 0.0 0. 0. 0. 0.

* REAR PASS

701500 28 2 4876800. 2859.699951 1. 1.

701501 0. 0. 0. 0. 0. 0.

701502	0.	0.	0.0	0.	0.						
* SUPERHEATER HORIZONTAL ASSEMBLIES											
701600	28	1	3500000.	2859.699951	909.						
701604	3	0	2	31.75	52.25	31.25	20.				
701605	156.	5.	1.48	2.	4.	4.	0.				
701606	0.	0.9	20.	0.	0.000135	0.					
701607	0.	62738.	0.	0.	0.	0.					
701608	0.	0.	0.0	0.	0.	0.	0.				
* ECONOMIZER											
701700	28	1	3360000.	2859.699951	483.						
701704	3	0	2	31.75	52.25	31.25	30.				
701705	178.	15.	1.6	2.	5.	3.5	861.75				
701706	882.5	0.9	20.	0.	0.000125	0.					
701707	0.	143705.	0.	0.	0.	0.	0.				
701708	0.	0.	0.0	0.	0.	0.	0.				
* AIR HEATER											
700500	21	2	601.	0.	0.	0.					
700501	0.	0.	0.	0.	0.						
700502	0.	0.	0.	0.	0.						
700503	0.	311000.	0.	0.	0.	0.	0.	0.	0.	0.	0.
* LEFT SIDE WATERWALL											
702800	29	1	70								
702804	0.2	1	171.5	208.	1.						
702805	1.56	2.	2.375	0.	0.	20.					
702806	0.000125	0.	0.	0.	6970.	0.					
702807	0.	0.	0.	0.	0.	0.					
* RIGHT SIDE WATERWALL											
702900	29	1	70								
702904	0.2	1	171.5	208.	1.						
702905	1.56	2.	2.375	0.	0.	20.					
702906	0.000125	0.	0.	0.	6970.	0.					
702907	0.	0.	0.	0.	0.	0.					
* FRONT WATERWALL											
703000	29	1	70								
703004	0.2	1	171.5	307.	1.						
703005	1.56	2.	2.375	0.	0.	20.					
703006	0.000125	0.	0.	0.	8934.	0.					
703007	0.	0.	0.	0.	0.	0.					
* REAR WATERWALL											
703100	29	1	70								
703104	0.2	1	171.5	307.	1.						
703105	1.56	2.	2.375	0.	0.	20.					
703106	0.000125	0.	0.	0.	8934.	0.					
703107	0.	0.	0.	0.	0.	0.					
* SUPHTR DIV PANELS											
704300	29	1	70								
704304	931.	1	50.	804.	2.						
704305	1.344	1.75	2.125	0.	0.	20.					
704306	0.000149	0.	0.	0.	13950.	0.					
704307	0.	0.	0.	0.	0.	0.4					
* SUPHTR PLATEN											
704400	29	1	70								
704404	925.	1	50.	714.	2.						
704405	1.594	2.	2.375	0.	0.	20.					
704406	0.000123	0.	0.	0.	13715.	0.					
704407	0.	0.	0.	0.	0.	0.4					
* RHTR RAD WALLS											
704900	29	1	70								
704904	680.	1	50.25	458.	1.						
704905	2.025	2.355	2.375	0.	0.	20.					

704906 9.87e-5 0. 0. 5104. 0.
 704907 0. 0. 0. 0. 0. 0.4

*

***** SOURCES, SINKS, AND VALVES

*

* AIR

700100 31 80. 14.7 4400000. 0. 0.

700103 AIR, -0.013

* FEEDWATER

702100 33 483. 2859.699951 3360000. 0. 0.

* SUPERHEAT SPRAY

704100 31 483. 2859.699951 140000. 0. 0.

* COLD REHEAT

704600 31 627. 595.700012 3120000. 0. 0.

* REHEAT SPRAY

704800 31 483. 2859.699951 0. 0. 0.

* DESIGN FUEL

705200 31 80. 2500. 409700. 0. 0.

705203 FUEL, 11315., SSVL, 0., CO2, 0., H2O, 0.1187

705204 SO2, 0., O2, 0.0867, N2, 0.0073, CO, 0.

705205 H2, 0.0451, C, 0.6198, S, 0.0338, ASH, 0.0886

* STEAM COIL INLET

705400 31 1.05 14.7 30000. 0. 0.

* STACK OUTLET

702000 30

* MAIN STEAM OUT

704500 32

* HOT REHEAT

705000 30

* BLOWDOWN

705100 30

* BOTTOM ASH

705300 30

* STEAM COIL OUTLET

705500 30

* TOP ASH

705600 30

*

***** PUMPS, COMPRESSORS, AND FANS

*

* MAIN CIRC PUMP - SET PUMP HEAD

702400 41 0. 1. 1. 0.82

702401 0. 0. 0. 0. 0. 223.

* F.D. FAN (80% EFFICIENCY ASSUMED)

700300 43 14.7 1. 1. 0.8

* I.D. FAN (80% EFFICIENCY ASSUMED)

701900 43 14.7 1. 1. 0.8

*

***** MIXERS

*

*

703600 50 1 0.

* SUPERHEAT SPRAY + MAIN STEAM

704200 50 1 0.

* REHEAT SPRAY + COLD REHEAT

704700 50 1 0.

* PREHEATED AIR + TEMPERING AIR

700600 50 1 0.

* REAR WW HANGER TUBES + RWV SCREEN TUBES

703300 50 0 0.

* WATER WALL MIXERS

703400 50 1 0.

*

703500 50 1 0.

*

***** SPLITTERS

*

* TEMPERING AIR

700400 61 0. 383300.

* R WW SCREEN TUBES, SPLIT PER FLOW AREA

703200 63 0. 0.29

* TOP ASH

701800 69 0. 0. 0.

701801 RCO2, 0., RH2O, 0., RSO2, 0., RO2, 0.

701802 RN2, 0., RCO, 0., RH2, 0., RC, 0.995

701803 RS, 0., RASH, 0.995

* F,R WALL (SPLIT PER FLOW AREA FRACTIONS)

702500 63 0. 0.725

* SIDE WALL

702600 63 0. 0.5

* REAR WALL

702700 63 0. 0.5

*

***** CLASS 7 COMPONENTS

*

* FURNACE/COMBUSTOR

700700 70 1 3 10 0.2

700701 0. 0. 0. 0.0018 0.0025 0.

700702 1. 100. 0. 0. 0. 0. 0.015

* BOILER DRUM

702300 73 1 520 2839.699951 0. 0. 0.

702301 5. 0. 0. 0.

702309 5 0 0. 0. 0.

*

*

* SPECIAL FEATURES

*

***** CONTROL BLOCKS

*

*

* SET CONTROL BLOCK ON ALL CONTROLS PRESENT

845100 1 2 3 4 0

846101 0. 0. 0. 0. 0.

846104 0. 0. 0. 0. 0.

*

***** OPERATIONAL VARIABLES

*

* FRACTION OF CONV. PASS HEAT TRANS. AREA, EXT. SIDE WALL

870030 0.006

* FRACTION OF CONV. PASS HEAT TRANS. AREA, REAR PASS

870040 0.044

*

***** OPERATIONS

*

* SET BOILER EFF. FLUE GAS TEMPERATURE

880010 TTUNCT 50 EQL ETTFG 1

* SET FURNACE COMPONENT INPUT WORD FOR HEAT LOSSES

880020 ELUNSP 1 EQL UFUNL 70

```

* SET FURNACE INPUT WORD FOR FRACTIONAL UNACC. HEAT LOSS
880030   OPVB      6   SUB   WWVSC   410   WWVSC   210
* SET FEEDWATER FLOW
880040   WWVSC    210  ADD   WW      232   WWVSC   210
* SET COLD REHEAT FLOW
880050   OPVB      7   SUB   WWVSC   480   WWVSC   460
* HEAT OUTPUT
880100   BBSTRM   131  ADD   BBSTRM  101   OPVB    10
*
880110   OPVB      10  ADD   BBSTRM  232   OPVB    10
*
880120   OPVB      10  SUB   BBSTRM  210   OPVB    10
*
880130   OPVB      10  SUB   BBSTRM  410   OPVB    10
*
880140   OPVB      10  SUB   BBSTRM  460   OPVB    10
*
880150   OPVB      10  SUB   BBSTRM  480   OPVB    10
* ENERGY INPUT
880300   QHHVFL    0   ADD   QHBAE    0   OPVB    20
*
880310   OPVB      20  ADD   QHBZE    0   OPVB    20
*
880320   OPVB      20  ADD   QHBFE    0   OPVB    20
*
880330   OPVB      20  ADD   QHBX     0   OPVB    20
*
880340   OPVB      20  ADD   QHBMAE   0   OPVB    20
*
880350   OPVB      20  ADD   QHBMIS   0   OPVB    20
* CALCULATE I/O EFF.
880400   OPVB      10  DIV   OPVB     20   OPVB    40
* CALC. TOTAL HEAT TO CONVECTIVE STAGES
881000   BBHXTS   80   EQL   OPVB    100
*
881010   BBHXTS   90   ADD   OPVB    100   OPVB    100
*
881020   BBHXTS  100   ADD   OPVB    100   OPVB    100
*
881030   BBHXTS  110   ADD   OPVB    100   OPVB    100
*
881040   BBHXTS  130   ADD   OPVB    100   OPVB    100
*
881050   BBHXTS  140   ADD   OPVB    100   OPVB    100
*
881060   BBHXTS  160   ADD   OPVB    100   OPVB    100
*
881070   BBHXTS  170   ADD   OPVB    100   OPVB    100
* CALC. EXT. SIDE WALL HEAT DUTY
881090   OPVB    100   MUL   OPVB     3   BBHXGR  120
881095      8
* CALC. REAR PASS HEAT DUTY
881100   OPVB    100   MUL   OPVB     4   BBHXGR  150
881105      8
*
***** SPECIAL INPUT/OUTPUT
*
890020   'MAIN STEAM (EVAPORATION) FLOW'
890021   OPVB      6   3500000.   I
890030   'HOT REHEAT FLOW'

```

```

890031      OPVB          7          3120000.      I
890040      'SUPERHEAT SPRAY FLOW'
890041      WWVSC         410         140000.      I
890050      'REHEAT SPRAY FLOW'
890051      WWVSC         200          0.          I
890060      'FUEL FIRING RATE'
890061      WWVSC         520         409700.      I
891010      'UNCORRECTED GAS EXIT TEMP.'
891011      TTUNCT        50
891020      'BOILER EFF BY I/O METHOD'
891021      OPVB          40
891030      'BOILER EFF BY HT LOSS METHOD'
891031      EFBLRD        0

```

```

*
***** BOILER EFFICIENCY CALCULATION
*

```

```

900000      1  100.  14.7
* FLUE GAS DESCRIPTION
900110      170   0.   0.   0.   0.   0.   0.
900111      0.   0.   0.   0.   0.   0.
* COMBUSTION AIR
900210      40   0.   0.   0.   0.
* FUEL DESCRIPTION
900310      520   0.   0.   0.   0.
900311      0.   0.   0.   0.   0.
* TEMPERING AIR
900510      41   0.   0.   0.   0.
* AUXILIARY DRIVE HEAT CREDIT - CIRC. PUMP
900610      240   0.
* UNBURNED CARBON IN STACK
901110      70   0.   0.
* UNBURNED CARBON IN REFUSE
901120      71   0.   0.
* RADIATION LOSS
901610      70   0.
* UNACCOUNTED HEAT LOSS
901910      0.0155

```

```

*
*
*
= (DPW) CONTROL SYSTEM BOILER MODEL
*

```

```

* CONTAINS THE TUNING FACTORS, BUT NOT THE CONTROLS, FROM THE FINE-TUNE
* STEP. NOW THE BOILER CONTROLS TO ACHIEVE EVAPORATION, AND MAIN
* STEAM AND REHEAT SET POINTS ARE INCLUDED. THE ROTARY AIR HEATER IS
* IN THE REFERENCE-BASED PREDICTIVE HEAT TRANSFER CALC MODE.
*

```

```

*****
*
*   GENERIC INPUT DATA
*
*****

```

```

* CYCLE CONVERGENCE DATA
012000      150   0.   0.   0.   0.   0.   10  500000.

```

```

* SPECIAL FEATURES INITIATION DATA
012001      5     2    10    0    0    0

```

```

* SPECIAL FEATURES CALCULATIONAL ORDER DATA
012002      0     0    0

```

```

*
*
*****
*      COMPONENT DATA
*****
*
***** HEAT EXCHANGERS
*
* AIR HEATER - REF-BASED PRED, HT MODE
700500   21     3
700503   0.  600000.   0.   0.   0.   0.   0.   0.   0.
700504  102.  601.  670.  268.  3819000.  4612000.
700506   0.   0.   0.   0.   0.   0.
*
***** SOURCES, SINKS, AND VALVES
*
* DESIGN FUEL
705200   31    80.  2500.  409700.   0.   0.
*
***** CLASS 7 COMPONENTS
*
* FURNACE/COMBUSTOR
700700   70     1     3     10    0.2
700701  2000.   0.   0.  0.0018  0.0025   0.
700702   1.  100.   0.   0.   0.   0.  0.015
* BOILER DRUM - ZERO DEMAND REF
702300   73     1     0  2839.699951   0.   0.   0.
702301   5.   0.   0.   0.
702309   5     0     0.   0.   0.
*
*
*****
*      SPECIAL FEATURES
*****
*
***** CONTROLS
*
* CONTROL FIRING FOR DRUM ENERGY IMBALANCE
840100  WWVSC   520   1.  100000.   1.  BBEIBC  230
840109  200000.  900000.
*
* CONTROL FURNACE EXIT T FOR HOT REHEAT
840200  TEXTF   70  1005.  1e-4   1.  TT      101
840209  1200.  2700.
*
* CONTROL SH SPRAY FOR MAIN STEAM T
840300  WWVSC   410  1005.  1e-4   1.  TT      131
840309   0.  1200000.
*
* CONTROL DRUM P FOR MAIN STEAM P
840400  PPDRUM  230  2639.699951  1e-4   1.  PP      131
840409  2000.  3000.
*
***** CONTROL BLOCKS
*
*
* SET CONTROL BLOCK ON ALL CONTROLS PRESENT
845100   1     2     3     4     0
845108  KEEP

```

846101	0.	0.	0.	0.	0.
846104	0.	0.	0.	0.	0.

*
***** SPECIAL INPUT/OUTPUT

890060	'FUEL FIRING RATE'				
890061	WWVSC	520	575000.		I
891510	''				
891511	TEXF	70	2629.800049		I
891520	''				
891521	RSVF	430	0.4		I
891530	''				
891531	RSVF	440	0.4		I
891540	''				
891541	RSVF	490	0.4		I
891550	''				
891551	HTTIRH	80	-0.3		I
891560	''				
891561	HTTIRH	100	-0.31		I
891570	''				
891571	HTTIRH	130	-0.73		I
891580	''				
891581	HTTIRH	140	-0.85		I
891590	''				
891591	HTTIRH	160	-0.85		I
891600	''				
891601	HTTIRH	170	-0.75		I
891610	''				
891611	TUFORM	80	-1.		I
891620	''				
891621	TUFORM	100	-8.75		I
891630	''				
891631	PDHXTU	150	0.01		I
891640	''				
891641	TUFORM	130	-6.875		I
891650	''				
891651	TUFORM	140	-1.		I
891660	''				
891661	TUFORM	160	-1.		I
891670	''				
891671	TUFORM	170	-5.		I
891680	''				
891681	TUFORM	430	-1.		I
891690	''				
891691	TUFORM	440	-1.		I
891700	''				
891701	FRMLS	490	-1.		I
891710	''				
891711	TUFORM	280	-1.		I
891720	''				
891721	TUFORM	290	-1.		I
891730	''				
891731	TUFORM	300	-1.		I
891740	''				
891741	TUFORM	90	-1.		I
891750	''				
891751	TUFORM	110	-1.		I
891760	''				
891761	PDHXTU	120	0.01		I
891770	''				

891771	TUFORM	310	-1.	I
891780	''			
891781	HTTIRH	90	-0.85	I
891790	''			
891791	HTTIRH	110	-0.85	I

*
*
*
*

* COMPONENT DATA

* SOURCES, SINKS, AND VALVES

* BLACK THUNDER

705200	31	80.	2500.	575000.	0.	0.		
705203	FUEL,	8800.,	SSVL,	0.,	CO2,	0.,	H2O,	0.28
705204	SO2,	0.,	O2,	0.1252,	N2,	0.0069,	CO,	0.
705205	H2,	0.0354,	C,	0.5,	S,	0.0034,	ASH,	0.049

*
*

* SPECIAL FEATURES

* SPECIAL INPUT/OUTPUT

890010	'FUEL FIRING RATE'			
890011	WWVSC	520	575000.	I

*
*
*
*

* END OF BASE DECK

*
*
*